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Subject: Hope Bay Project: Summary of 3-D Hydrodynamic Modelling Study of Roberts Bay

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1.0 INTRODUCTION

Tetra Tech Canada Inc. (Tetra Tech) has been retained by Agnico Eagle Mines Limited (Agnico Eagle) to develop and conduct a three-dimensional (3-D) hydrodynamic modelling study of Roberts Bay to quantify effluent concentrations and dilutions at the edge of the mixing zone.

Hope Bay is a gold mining and exploration Project located on a property approximately 20-km × 80-km along the south shore of Melville Sound (called Roberts Bay) in Nunavut, Canada. It continued to be operated by TMAC Resources Inc. (TMAC). On February 2, 2021, TMAC was purchased by Agnico Eagle and became a wholly owned subsidiary of Agnico Eagle. Commercial production began in 2017 and continued until February 18, 2022, when it was announced that the mine would be placed into temporary Care and Maintenance.

Agnico Eagle is planning to restart operations, which includes refinements to the approved Doris and Madrid areas that were previously assessed in the 2017 Final Environmental Impact Statement (FEIS; TMAC 2017) and approved by the Nunavut Impact Review Board (NIRB), to further enhance the Hope Bay Mine plan. The refinements to the operations relevant to this modelling study include:

- Increased generator capacity at Doris and Madrid, to support increased mill rate of 2,400 tonnes per day (tpd) to 8,000 tpd;
- Phased transition from slurry to dry stack/filtered tailings at the Tailings Impoundment Area; and
- Installation of a second diffuser in Roberts Bay for segregation of water.

2.0 METHODOLOGY

Roberts Bay 3-D ocean model was developed with Tetra Tech's proprietary 3-D hydrodynamic/coastal model (Stronach et al., 1993; Stronach et al., 2002; Stronach et al., 2015) embedded with the US-EPA Visual Plumes model (Frick, W.E. et al, 2004). The advantage of this modelling framework lies in the fact that it allows to assess both near- and far-field effluent discharge fate and transport over multi-years; therefore, accounting for effluent accumulation over time in Roberts Bay. In other words, it incorporates both the initial mixing and transport associated with the near-field, as well as a defensible far-field behavior in the entire bay driven by environmental conditions and ocean physical processes. Therefore, this modelling approach allows to characterize a more complete view and obtain more accurate results of the effluent transport and mixing in the ocean.

Figure 1 presents the 3-D Roberts Bay model domain and bathymetry. The bathymetry data was provided by Agnico Eagle based on bathymetry survey, and then interpolated onto the 3-D Roberts Bay model domain. The locations of the two diffusers were denoted as green (existing diffuser) and pink (proposed diffuser) dots in Figure 2.1.

A sea ice module has been developed and integrated into the 3-D hydrodynamic modeling framework. Several environmental data and forcings were employed in the 3-D Roberts Bay modelling study:

- Hourly wind and meteorological data at Doris site from 2019 to 2023, representative of the Roberts Bay meteorological conditions as provided by Agnico Eagle;
- Tidal components extracted from TOPEX/Poseidon Global Inversion Solution TPXO Tidal Model Driver (TMD) Database (Egbert and Erofeeva, 2002) to force onto the 3-D Roberts Bay model open boundaries;
- Monthly temperature and salinity profiles extracted from HYCOM Global Ocean Model forecasting system and observed measurements in Roberts Bay provided by Rescan (Rescan, 2010; Rescan 2011; Rescan 2012) to apply onto the open boundaries of the 3-D Roberts Bay model; and
- Daily river flows discharging into Roberts Bay based on measurements from ERM (ERM, 2022; ERM, 2024) – Little Roberts River (2019-2023) and Glenn River (2012-2014, 2019-2023).

The existing diffuser is located at (431,965 m E, 7,564,961 m N UTM Zone 13W) at a water depth of 17 m relative to NAD 83 projection datum. The proposed diffuser is expected to follow the same corridor as the existing outfall and is proposed to be located about 350-m northward of the existing diffuser. The coordinates for the proposed diffuser location are (431,967 m E, 7,565,315 m N UTM Zone 13W) located at a water depth of 31 m with respect to NAD 83 projection datum.

Two types of effluent are discharged through the two diffusers: the *Tailings Impoundment Area* (TIA) effluent and the *Saline Pond 1*(SP1) effluent. In this modelling study, the TIA effluent is discharged through the proposed diffuser and SP1 effluent is released from the existing diffuser to Roberts Bay. At present, this discharge configuration is considered optimal however, adjustments to the discharge strategy may be necessary based on further modeling work. Details of the diffuser configurations used in this modelling study are provided in Table 2.1.

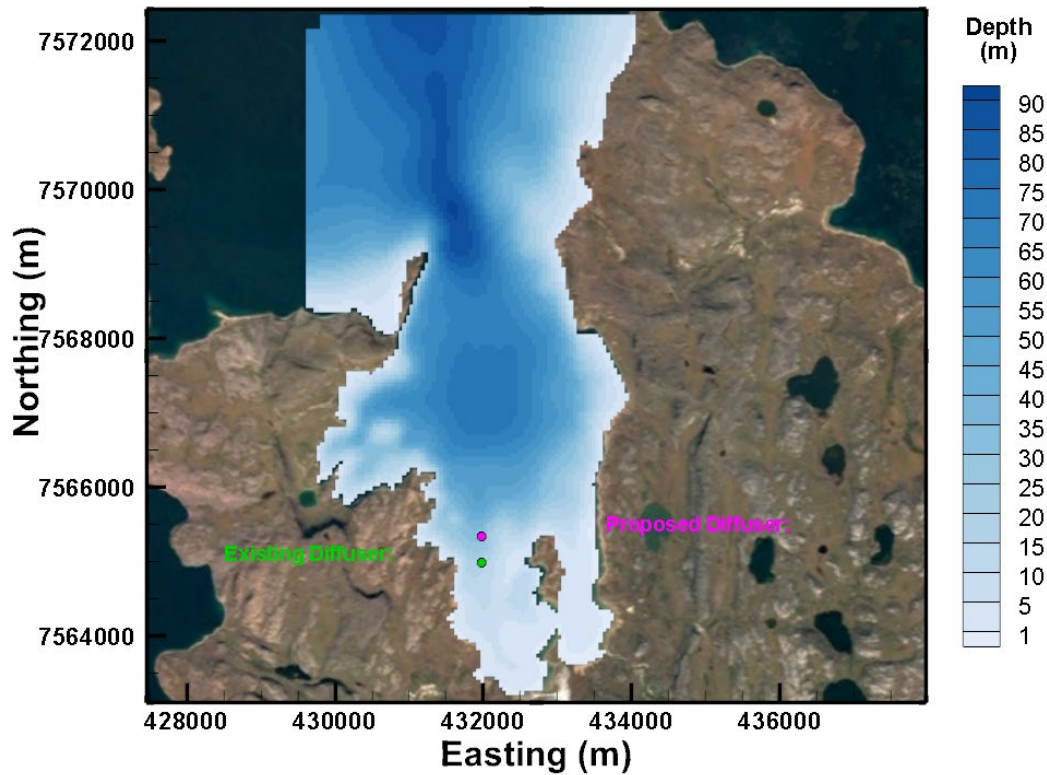


Figure 2.1: 3-D Roberts Bay Model Domain and Bathymetry. Green dot denotes existing diffuser location and pink dot denotes proposed diffuser location.

Table 2.1: Diffuser Configurations for Existing and Proposed Diffusers

Diffuser Specifications	Existing Diffuser	Proposed Diffuser
Coordinate of Location	431,965 m E, 7,564,961 m N UTM Zone 13W	431,967 m E, 7,565,315 m N UTM Zone 13W
Discharge Depth of Diffuser (m)	17.2	30.6
Number of Risers	4	2
Spacing Between Risers (m)	8.2	8.2
Number of Ports	8	4
Port Diameter (mm)	101.6	101.6
Port Height (m)	1.25	1.25
Vertical Angle of Port	0°	45°

3.0 MODEL VALIDATION

Model calibration and validation were conducted for the 3-D Roberts Bay modelling framework. A very good agreement was obtained between model results and observations in terms of i) water level, ii) sea ice formation and decay processes as well as ice thickness, iii) temperature and salinity distributions in the water column and their temporal (monthly) variations, and iv) ocean currents strengths and directions at different depths throughout different periods of the year.

4.0 HOPE BAY DISCHARGE SCENARIO DESCRIPTION

The Hope Bay effluent discharge scenario consists of a consecutive multiple-year simulation with year-round effluent discharge conditions at both diffusers (existing and proposed), starting from 2020 and finishing by end of 2041. Table 4.1 provides the summary of the different effluent discharge configurations through two diffusers. The discharge volumes and water quality parameters pertain to untreated effluent provided by SRK’s model predictions (SRK, 2024). On average, the TIA effluent exhibits a slightly higher discharge rate with about 127 m³/hr than the SP1 effluent with 100 m³/hr. Hence, the TIA effluent was assigned to the proposed diffuser located at a deeper water depth, with a reduced number of ports to reach an optimized exit port velocity. This discharge configuration is currently assumed to be optimal however, adjustments to the discharge strategy may be necessary based on further modeling work.

Table 4.1: Hope Bay Effluent Discharge Configurations for Existing and Proposed Diffusers

	Existing Diffuser	Proposed Diffuser
Effluent Type	SP1	TIA
Effluent Discharge Period	2028 – 2041 year-round	2020 – 2041 year-round
Effluent Discharge Rate (m³/hr)	Variable, from 78 to 124	Variable, from 0 to 396
Discharged Effluent TDS Concentration (mg/L)	Variable, from 771 to 7,626	Variable, from 60 to 7,135

To visualize, Figure 4.1 presents monthly discharged effluent volume and monthly untreated effluent TDS concentrations of TIA effluent through proposed diffuser over the entire discharge period. It is worth noting that effluent discharge rates from 2020 to 2024 do not reflect realistic past operations of discharge since no actual discharge continued after 2021. This discharge schedule is only a reflection of SRK’s model prediction results. Total volume of TIA effluent expected to release over the entire discharge period is approximately 25 Mm³.

Similarly, Figure 4.2 presents monthly discharged effluent volume and monthly untreated effluent TDS concentrations of SP1 effluent through the existing diffuser. SP1 effluent discharge occurred from year 2028 with a reduced discharge rate. Total volume of SP1 effluent expected to release over the entire discharge period is roughly 12 Mm³.

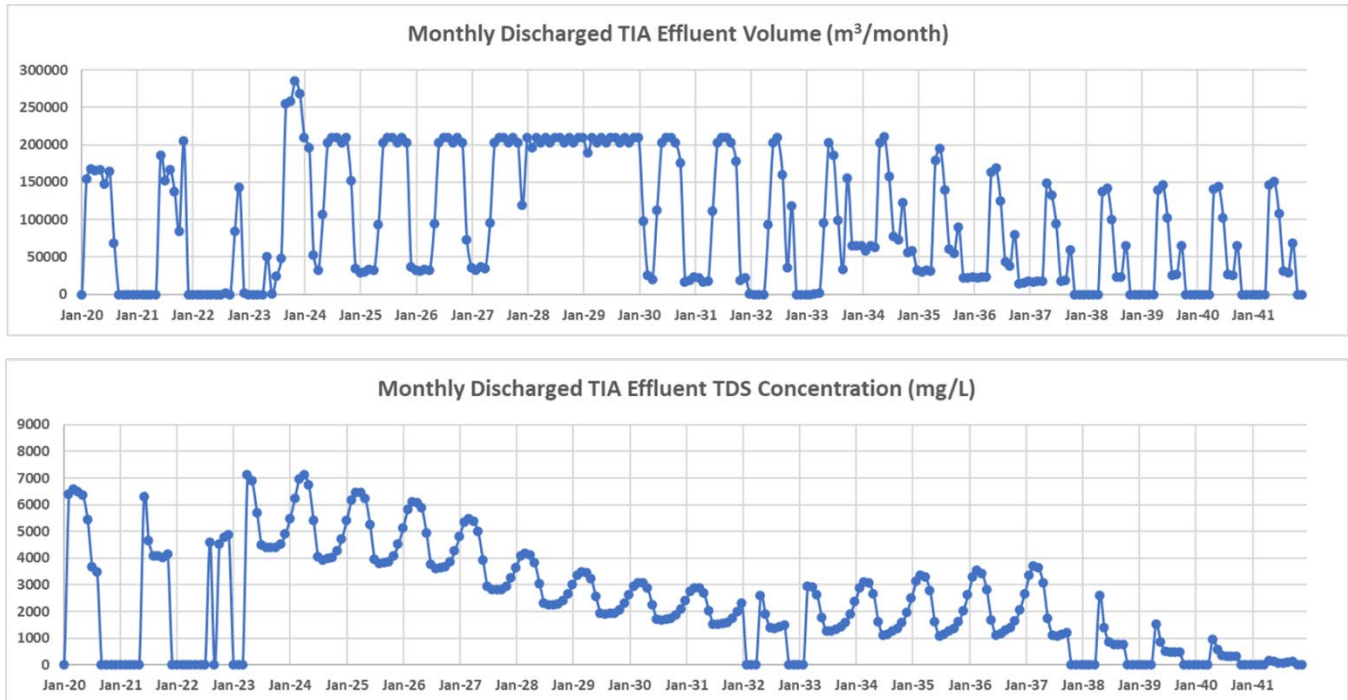


Figure 4.1: Monthly TIA Effluent Discharge Volume (Upper Panel) and Discharged TDS Concentration (Lower Panel) from Year 2020 to 2041 via the Proposed Diffuser

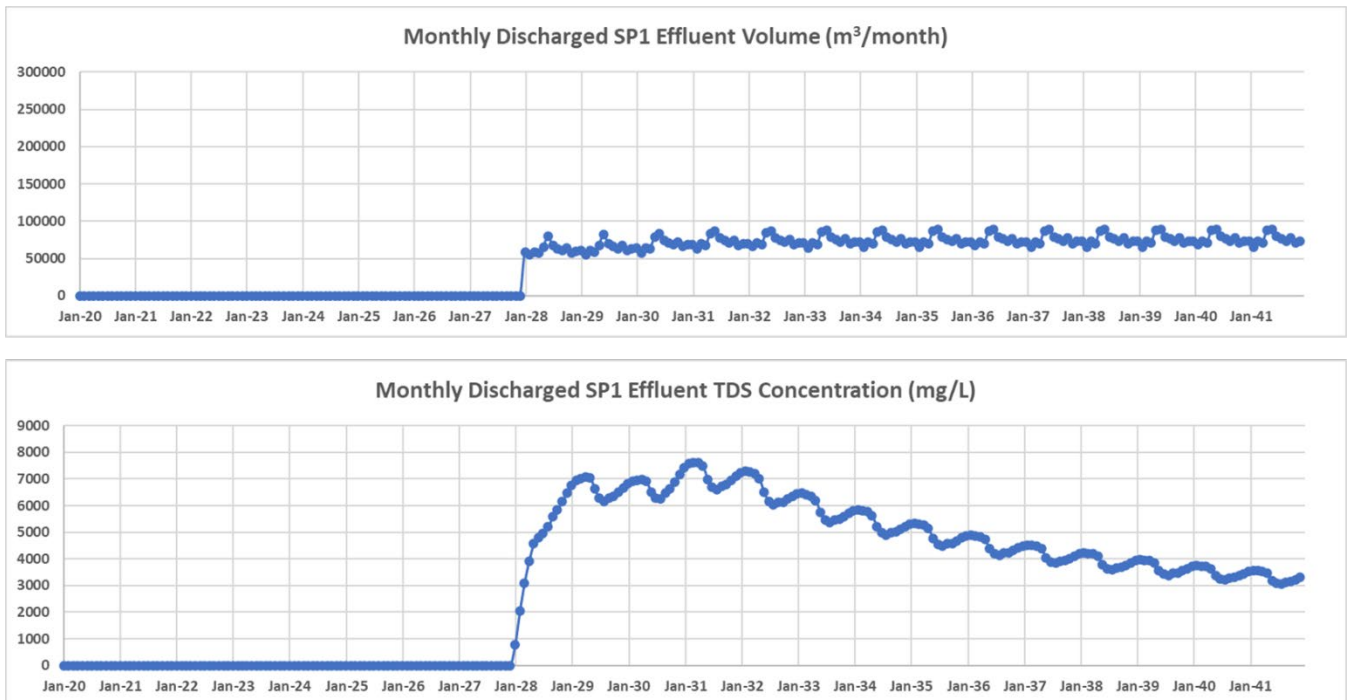


Figure 4.2: Monthly SP1 Effluent Discharge Volume (Upper Panel) and Discharged TDS Concentration (Lower Panel) from Year 2028 to 2041 via the Existing Diffuser

Table 4.1 presents monthly effluent temperature, based on empirical estimate from operations.

Table 4.1: Effluent Monthly Discharge Temperature

Month	Effluent Temperature (°C)
January	2
February	2
March	2
April	2
May	2
June	4
July	10
August	10
September	4
October	2
November	2
December	2

5.0 HOPE BAY SCENARIO MODELLING DILUTION RESULTS

Table 6.1 provides the statistics of modelled minimum and average dilution obtained at the MZB of the existing diffuser discharging SP1 effluent for each simulated year. **A conservative minimum dilution of 147:1 was reached at the MZB of the existing diffuser over the 22-year simulation.**

Table 6.1: Statistics of Minimum and Average Dilution Reached at the MZB of the Existing Diffuser with SP1 Discharge for Each Year

Simulated Year	Minimum Dilution Predicted at the MZB	Average Dilution Predicted at the MZB
2020	284:1	>10,000:1
2021	265:1	>40,000:1
2022	401:1	>200,000:1
2023	147:1	>100,000:1
2024	179:1	5,071:1
2025	189:1	6,084:1
2026	151:1	12,735:1
2027	262:1	5,946:1
2028	170:1	1,707:1
2029	151:1	1,266:1

Simulated Year	Minimum Dilution Predicted at the MZB	Average Dilution Predicted at the MZB
2030	155:1	1,626:1
2031	219:1	1,977:1
2032	316:1	2,190:1
2033	207:1	2169:1
2034	241:1	1,805:1
2035	280:1	1,919:1
2036	291:1	2,237:1
2037	284:1	2,736:1
2038	303:1	2,552:1
2039	282:1	2,132:1
2040	301:1	2,209:1
2041	259:1	2,562:1

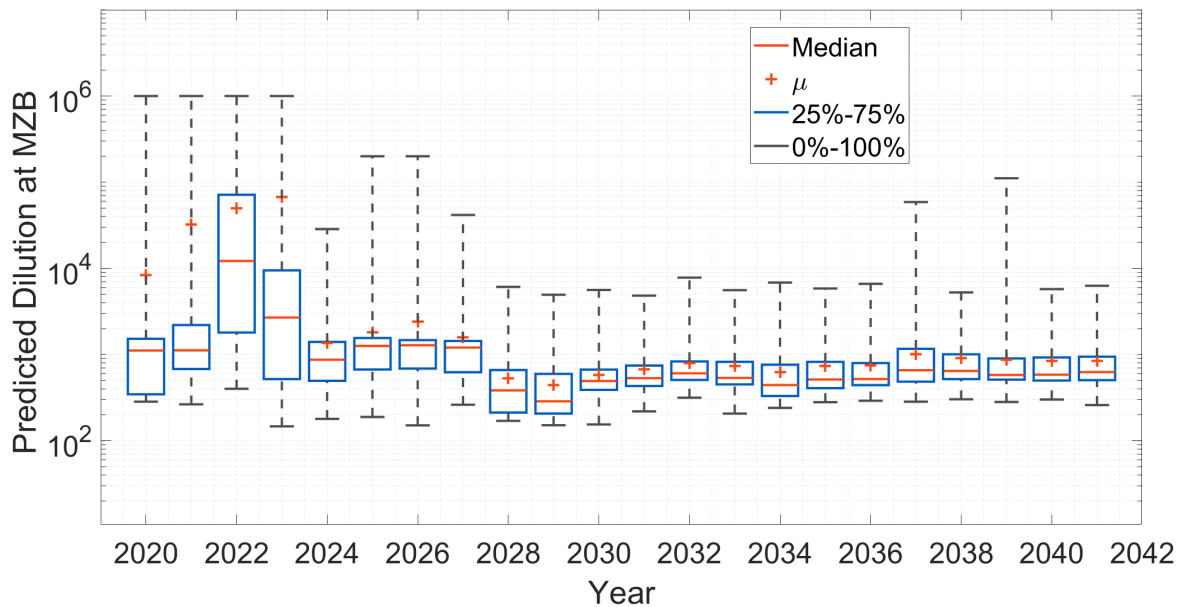


Figure 6.1: Box and Whisker Plot of Range of Minimum Dilutions Achieved at the MZB of Existing Diffuser from 2020 to 2041.

Figure 6.1 assembles the range of minimum dilutions obtained at the MZB of the existing diffuser discharging SP1 effluent in the form of box and whisker, including statistics of median, average, range of 25th-75th percentile and range of minimum and maximum of minimum dilutions of each year. A few findings were summarized below:

- From 2020 to 2027, much higher dilutions were obtained at the MZB due to the absence of SP1 effluent discharge and transport of TIA effluent carried by ocean currents; and

- From 2028 when SP1 effluent discharge kicks off, dilutions start to drop down (i.e. concentrations are increasing), reflecting a combined impact from both diffusers. Dilutions showed similar variability pattern during 2028-2041 discharge years, and the average dilution throughout each year fluctuated around a similar level at about 600:1.

Table 6.2 provides the statistics of modelled minimum and average dilution obtained at the MZB of the proposed diffuser discharging TIA effluent for each simulated year. **A conservative minimum dilution of 117:1 was reached at the MZB of the proposed diffuser over the 22-year simulation.**

Table 6.2: Statistics of Minimum and Average Dilution Reached at the MZB of the Proposed Diffuser with TIA Discharge for Each Year

Simulated Year	Minimum Dilution Predicted at the MZB	Average Dilution Predicted at the MZB
2020	237:1	>10,000:1
2021	170:1	>20,000:1
2022	280:1	>100,000:1
2023	117:1	>90,000:1
2024	129:1	2,976:1
2025	146:1	3,805:1
2026	128:1	3,728:1
2027	170:1	3,604:1
2028	134:1	1,483:1
2029	135:1	1,259:1
2030	137:1	2,079:1
2031	166:1	2,399:1
2032	343:1	3,273:1
2033	177:1	2,943:1
2034	242:1	2,813:1
2035	261:1	2,679:1
2036	310:1	3,177:1
2037	288:1	4,594:1
2038	316:1	4,031:1
2039	303:1	3,527:1
2040	322:1	3,573:1
2041	254:1	3,901:1

Figure 6.2 assembles the range of minimum dilutions obtained at the MZB of the proposed diffuser with TIA effluent discharge in the form of box and whisker, including statistics of median, average, range of 25th-75th percentile and range of minimum and maximum of minimum dilutions of each year. Several findings were described below:

- Much higher dilutions were predicted during year 2020-2023, due to a low volume of discharge with relatively sparse discharge frequency;
- Overall dilutions decreased in 2024 due to a significant increase in discharge volume from 0.8 Mm³ to 1.8 Mm³, which also resulted in a less intra-annual variability of dilution range;
- High volume of consecutive monthly discharge in 2029 considerably limited the dilutions, leading to the least dilution variability (i.e., from 135:1 to 1,615:1) compared to rest of the years; and
- Dilutions started to rise from 2030 and stabilized near 1,000:1 on average until the end of the simulation year of 2041, primarily due to the reduction of discharge volume over these years.

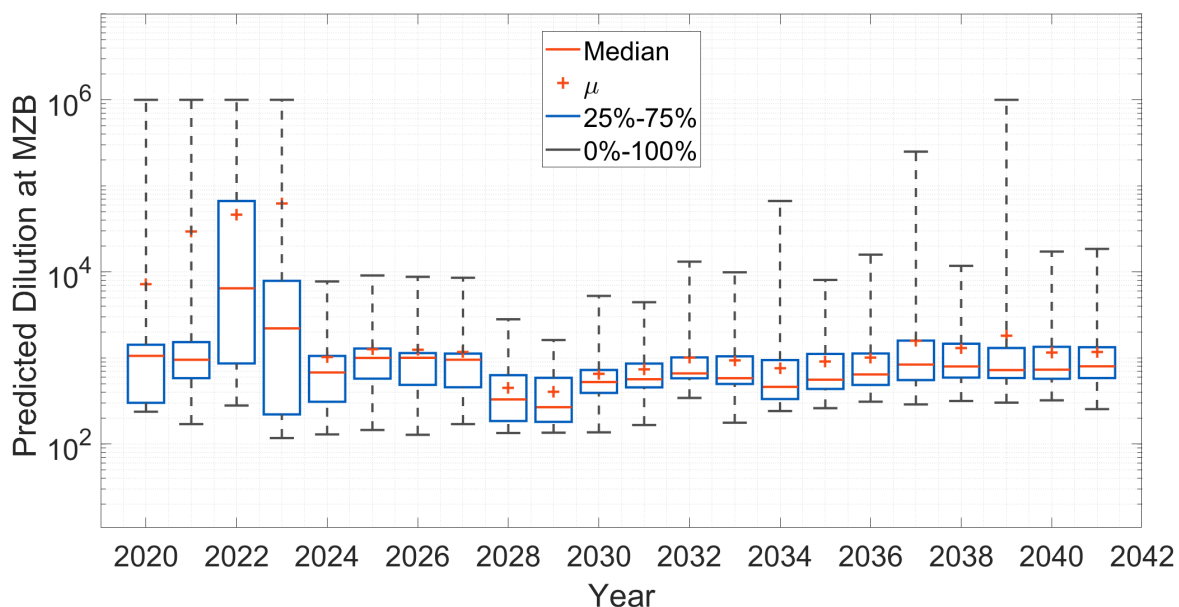


Figure 6.2: Box and Whisker Plot of Range of Minimum Dilutions Achieved at the MZB of Proposed Diffuser from 2020 to 2041.

6.0 CONCENTRATIONS OF CONTAMINANTS OF POTENTIAL CONCERN

Through the 3-D hydrodynamic model for Roberts Bay, predictions were made regarding the dilution of effluent upon reaching the mixing zone. Additionally, a comprehensive set of constituents was forecasted and utilized as input to the Human Health and Ecological Risk Assessment (HHERA) for the Hope Bay Operational Update (WSP 2025).

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We trust this technical memo meets your present requirements. If you have any questions or comments, please contact the undersigned.

Respectfully submitted,
Tetra Tech Canada Inc.



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