



Design Report Sewage Treatment Plant (STP) Upgrade

6526-460-132-REP-002

In Accordance with Licence 2AM-MEL1631 Part D, item 1 & 2

Prepared by:

Agnico Eagle Mines Limited – Meliadine Division



DOCUMENT CONTROL

Version	Date (YMD)	Section	Page	Revision
R0	17/07/2019			Design report

Prepared By:

2020-07-17

Thomas Genty

Water Treatment Eng.

OIQ 5021068

Approved by:

2020-07-17

Jessica Huza

Environment Superintendent





TABLE OF CONTENTS

1	INTRODUCTION	!
1.1	Site Location and Access	
1.2	Site Facilities	
1.3	Purpose of Document	
1.4	Scope of work	5
2	DESIGN METHODOLOGY	8
2.1	Design rationale, requirements, criteria and parameters	8
2.2	Design standards analysis and methods	
2.3	Design assumptions and limitations	
2.4	Waste water Charactisitics	8
2.5	Water Management Strategy	(
3	DESCRIPTION	9
3.1	Concept	
3.2	Flow equalisation and screening	
3.3	Aerobic reactor	
3.4	Membranne Filtration	10
3.5	UV disinfection	10
3.6	Sludge storage and dewatering	11
4	CONSTRUCTION METHODS	11
4.1	Construction method and equipment	11
4.2	Quality control/assurance	
4.3	Testing and inspection	11
4.4	Timeline	1 1



LIST OF FIGURES

Figure 1 : General location plan	. 7
LIST OF TABLES	
Table 1: Expected operational parameters	

LIST OF APPENDICES

Appendix A: STP Upgrade Drawings Appendix B: Current STP Drawings



1 INTRODUCTION

1.1 SITE LOCATION AND ACCESS

Agnico Eagle Mines Limited (Agnico Eagle) is developing the Meliadine gold mine located approximately 25 km north of Rankin Inlet, and 80 km southwest of Chesterfield Inlet in the Kivalliq Region of Nunavut. The project site is located on the peninsula between the East, South, and West basins of Meliadine Lake (63°01'23.8"N, 92°13'6.42"W). The area is accessible from the all-weather gravel road linking the Meliadine mine site with Rankin Inlet.

A general location plan for the project is shown in Figure 1.

1.2 SITE FACILITIES

The current mine plan focuses on the development of the Tiriganiaq gold deposit which will be mined using both conventional open-pit and underground mining operations. Current mining facilities to support the Mine include a plant site and accommodations, tailings storage facility, waste rock storage facilities, ore storage pads, process plant, power plant, maintenance facilities, water management treatment plants and supporting infrastructures.

Such infrastructures include water retention dikes, berms, culverts, channels, collection ponds, pumping stations, fresh water intake and water treatment plants are required to manage water during pre-production, operation, and interim mine closure.

To support the camp accommodation, upgrading the current sewage treatment (STP) plant unit would be required.

1.3 PURPOSE OF DOCUMENT

This report includes the final design and construction drawings for the STP upgrade.

1.4 SCOPE OF WORK

H2O innovation was selected to supply the STP upgrade. Construction drawings of the listed infrastructure are presented in appendices of this report. Note that the STP concept stays the same but an additional aerobic tank and membrane filtration unit are added.







2 DESIGN METHODOLOGY

2.1 DESIGN RATIONALE, REQUIREMENTS, CRITERIA AND PARAMETERS

The design rationales are the following:

- Provide additional sewage treatment capacity for the camp;
- Limit extent of required modifications of the current infrastructure;
- Ensure the system is containerized for simplicity.

Table 1 presents the target effluent concentration at the exit of the STP. Note that these parameters are operational targets and no effluent are discharged to the environment.

Table 1: Expected operational parameters

Parameter	Unit	Effluent target
BOD ₅	mg/L	<25
TSS	mg/L	<25
pH	units	6-9
Ammonia Nitrogen (N-NH3)	mg/L	0.89
Fats, Oils and Grease	mg/L	15

2.2 DESIGN STANDARDS ANALYSIS AND METHODS

STP upgrade equipment were selected to manage an equivalent of 200 additional people in the camp (the current STP is designed for 520 persons). The selection of each of these components was based on a typical process used in the industrial water treatment sector and synergy with the current STP set up was prioritized. The robustness and redundancy of equipment were also taken into account during equipment/supplier selection.

2.3 DESIGN ASSUMPTIONS AND LIMITATIONS

The current treatment plant is able to treat a maximum daily flow of 216 000 L per day (maximum design flow). The upgrade STP equipment will be able to handle an additional 83 076 L per day.

2.4 WASTE WATER CHARACTISITICS

Table 2 presents the raw sewage water characteristic used for the design.

Table 2: Raw Water

Table 2: Naw Water					
Parameter	Unit	Raw water			
BOD ₅	mg/L	200-360			
TSS	mg/L	50-350			
рН	unit	6.5-8.5			
Ammonia Nitrogen (N-NH3)	mg/L	40-50			
Fats, Oils and Grease	mg/L	20-50			
TKN	mg/L	45-60			
Ptotal	mg/L	5-12			
Alkalinity	mg/L	250-500			



2.5 WATER MANAGEMENT STRATEGY

Sewage will be collected from the facilities and pumped to the STP. The objective of the STP is to treat sewage to an acceptable level for discharge to CP1 via a sewage water discharge pipeline. The STP is housed in a prefabricated (modular) structure, located on the east side of the industrial pad (Figure 1).

The treated sewage from the STP will be pumped through a heat traced insulated pipeline to CP1 pond which is designed to receive all the surface contact waters on site. This water is pumped to the final effluent treatment plant for TSS control prior to discharge into Meliadine Lake.

The composition of the sewage and grey water entering the plant and the Effluent water quality exiting the units will be monitored on a regular basis to determine plant efficiency. Sewage sludge removed from the STP will be added to the landfarm as nutrient amendment, on an as needed basis. Excess sludge will be disposed of in the waste rock storage facility (WRSF) primarily, however alternate disposal options are possible such as the Tailings Storage Facility or shipment south for disposal.

3 DESCRIPTION

3.1 CONCEPT

The STP relies on bacterial activity. The process is composed of five (5) steps described below:

- flow equalization and screening,
- · aerobic biological treatment,
- membrane filtration,
- ultraviolet disinfection,
- and sludge handling/dewatering.

PIDs are available in appendices.

3.2 FLOW EQUALIZATION AND SCREENING

The influent wastewater is pumped to the two (2) aerated equalization tanks. The equalization system is able to manage a variation in flows. It provides raw wastewater storage to store feed during high flow periods and to ensure feed supplementation during low flow periods. It provides a stable and consistent raw feed for the downstream processes. Equalized water is pumped via two (2) equalization pumps into a standpipe inside the second tank and flows from that pipe by gravity to the fine screens. The fine screens are rotary drum screens with 2 mm perforated plate openings that operate continuously. The screens will ensure the removal of large debris to protect downstream equipment. Pressurized wash water is used intermittently to clean the screens and screenings.

3.3 AEROBIC REACTOR

Screened raw water flows by gravity from the screens into the sump tank, where it is pumped to the aerobic tank, which is located outdoors. Aerobic biological treatment removes the organic load (measured as BOD) of the wastewater. Bacteria grown in the bioreactor remove unwanted organic pollutants to produce a treated water of high quality. Oxygen is supplied by regenerative blowers and is injected by fine bubble diffusers in the tank. The diffusers are designed for a wide range of air flows, according to the system's demand in oxygen. It keeps a dissolved oxygen concentration of at least 2 mg/L at any time to satisfy the needs of the biomass. The mixed liquor suspended solids (MLSS)



overflows into a standpipe inside the tank and flows by gravity to the membrane filtration trains. The target MLSS in the aerobic reactor is 10 g/L.

The dry bacteria product, BEC105, could be used in the treatment process to stimulate biological activity when needed. To start up of the new bioreactor, sludge from the current plant can be used too.

The equipment added in the STP upgrade is an aerobic tank with fine bubble diffusor.

3.4 MEMBRANE FILTRATION

Membrane filtration is used to separate the bacteria from the water to ensure keeping them in the process at the desired concentration. Activated sludge is returned at a constant flow rate to the aerobic tank to prevent a build-up of sludge in the membrane tank. The return activated sludge (RAS) is pumped at a higher flow rate than the design flow rate of the plant, to make sure that there is good circulation in the whole system and that there is no accumulation of solids.

The membranes are totally submerged and have a pore size of 0.4 microns, which remove all suspended solids in the effluent.

The permeation pumps are provided to suction the effluent through the membrane modules and transport it to the permeate tank. The permeation pumps are supplied with variable speed drives to overcome any changes in transmembrane pressure and achieve the design at all times.

The operating cycle for the selected modules is to suction effluent water for seven (7) minutes and to relax the membrane for one (1) minute. The cycle optimizes the long-term operation of the membrane modules. The housings are constructed with an integrated diffuser at the bottom to aerate the membrane continuously and prevent clogging and accumulation of sludge. The relaxation of the membranes allows extending the interval between cleanings (CIP or Clean-In- Place). CIP cleans are done about twice a year. Washes are performed with permeate stored in the permeate storage tank while a cleaning chemical (either sodium hypochlorite or citric acid) is added. Chemical solutions are backflushed through the membranes, which are soaked for a few hours after. After washing, the permeation is restarted. While a train is washing, the other train can continue to treat water and ensure a continuous production of effluent.

Once a week, a chemically enhanced back pulse (CEB) should be performed on the membrane modules with sodium hypochlorite to mitigate membrane fouling. Permeate flow is reversed to flow back into the membranes while the cleaning chemical is added inline.

An additional sea can with a membrane train and utilities (instrumentation, blower, pumps, UV, CIP tank, sodium hypochlorite system) are added to the current STP system. This allows the filtration area to increase from 900 m² (current system) to 1350 m² (upgraded system).

3.5 UV DISINFECTION

From the permeate pumps, each membrane bioreactor train sends permeate through an inline ultraviolet disinfection system. It is a physical process that inactivates instantaneously microorganisms. The UV system process adds no chemicals to the water, and therefore, has no impact on the chemical composition of the effluent. From here, effluent is sent to a common permeate storage tank. The permeate tank acts as a reservoir for treated water that is pumped to the discharge location. This tank can also be used for CEB and CIP process, as previously mentioned.



3.6 SLUDGE STORAGE AND DEWATERING

Since bacteria continue to reproduce as they consume organics and nutrients, the concentration of biomass, measured as Mixed Liquor Suspended Solids (MLSS), increases with time. Periodic sludge wasting is required to control the MLSS concentration in the bioreactor tanks. Sludge is sent to the sludge storage tank by redirecting the flow of the RAS pump (approximately at 1% solid content). A blower and coarse bubble diffuser system maintains an aerobic environment within the sludge tank to minimize the proliferation of odors. Periodic settling is used to facilitate the thickening of the waste activated sludge. The supernatant (upper portion of the tank) is sent back to the sump tank by opening a valve, where it will re-enter the treatment process. This operation (called decanting) reduces the volume of sludge that needs to be handled and extends the period of time that the sludge tank can be used before thickened sludge is disposed (approximately at 2-3 % solid content).

A Sludge Dewatering System (Volute) system is also available to remove the solid fraction out of the sludge storage tank. Basically, the flocculated sludge pass through a screw press that utilizes a screw inside a moving casing. Water collected during the dewatering is sent back to the STP equalization tank. The cake is then collected in a solid-waste bin for disposal in the Waste Rock Storage Facility. Alternative disposal locations can include: Tailings Storage Facility, use at the landfarm as nutrient amendment or shipment south during the barge season for disposal. The system is designed to treat 3 to 5 m³ per 12 h and will produce approximately 0.28 m³ per day of sludge cake at approximately 18% solid. The cationic polymer consumption is estimated at 0.5 kg per day.

4 CONSTRUCTION METHODS

4.1 CONSTRUCTION METHOD AND EQUIPMENT

No building construction is expected for the upgrade. An additional container and tank will be placed close to the current infrastructure. Installation of equipment will be done on the existing industrial pad.

4.2 QUALITY CONTROL/ASSURANCE

A record of as-built drawings will be produced.

4.3 TESTING AND INSPECTION

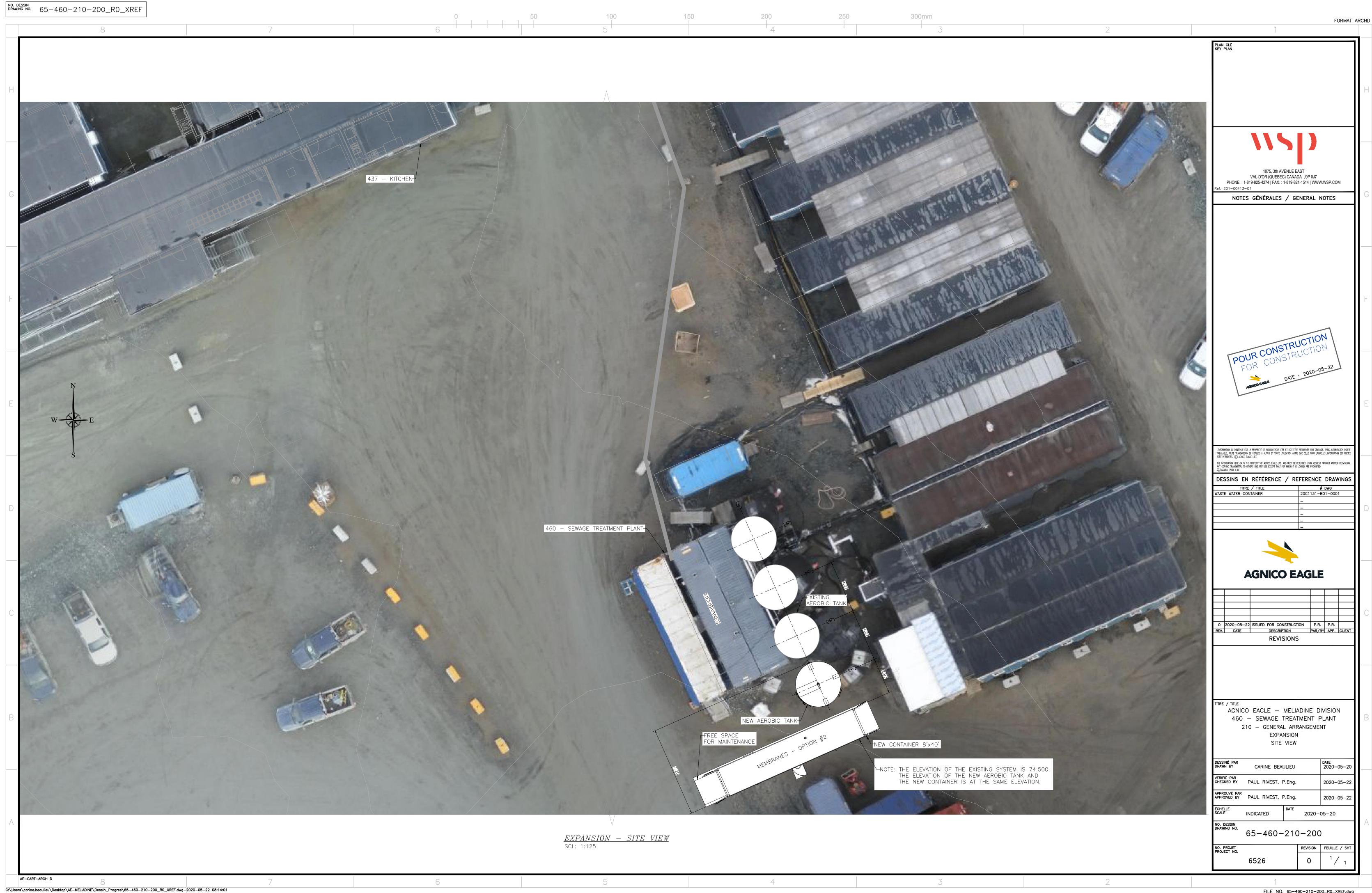
Prior to start up, the indoor pipe will be tested for leaks. If leaks are found, the pipe will be repaired.

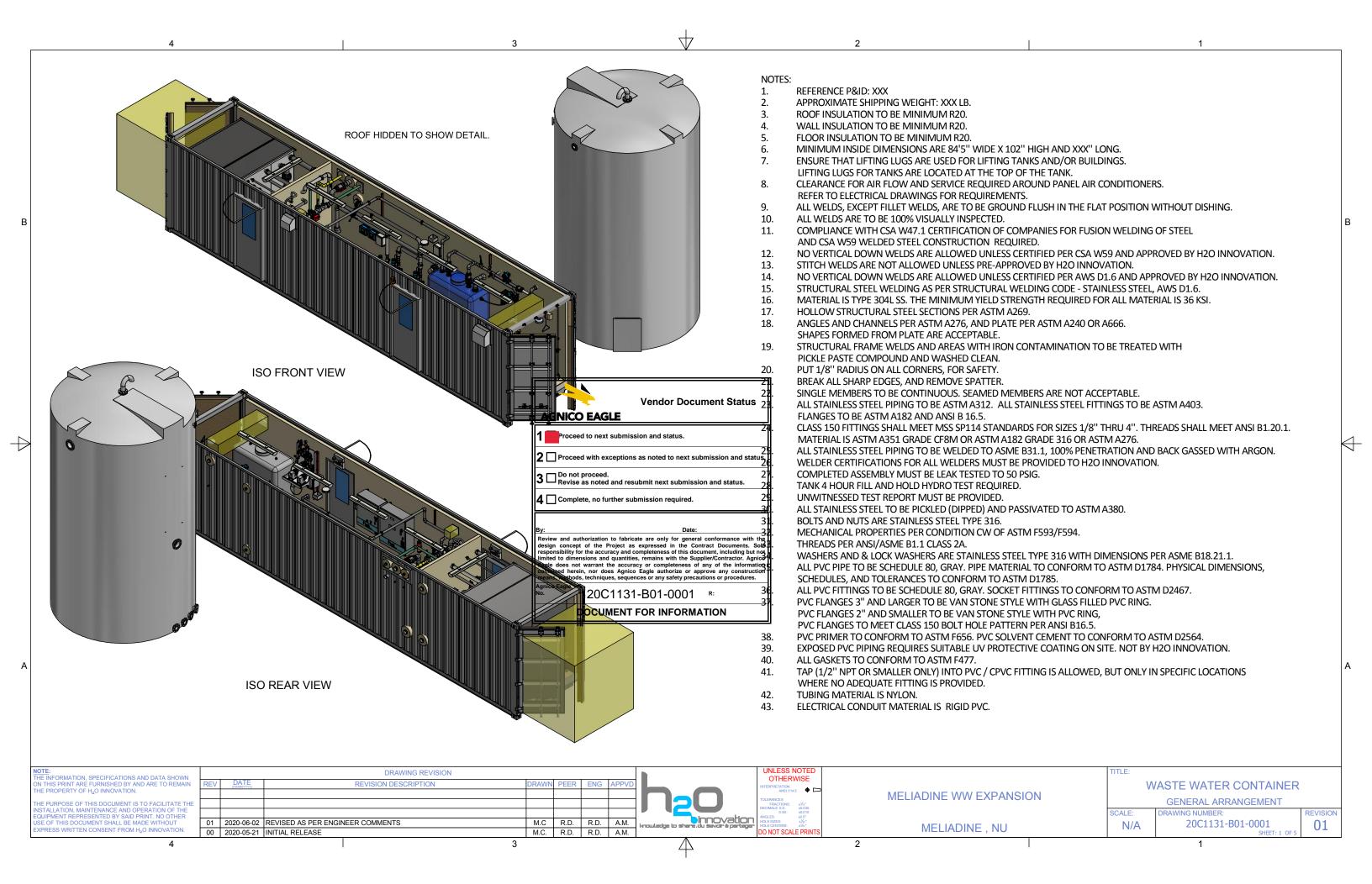
After start up, a periodic inspection, performed by Agnico Eagle personnel, will be done to ensure piping and plant integrity.

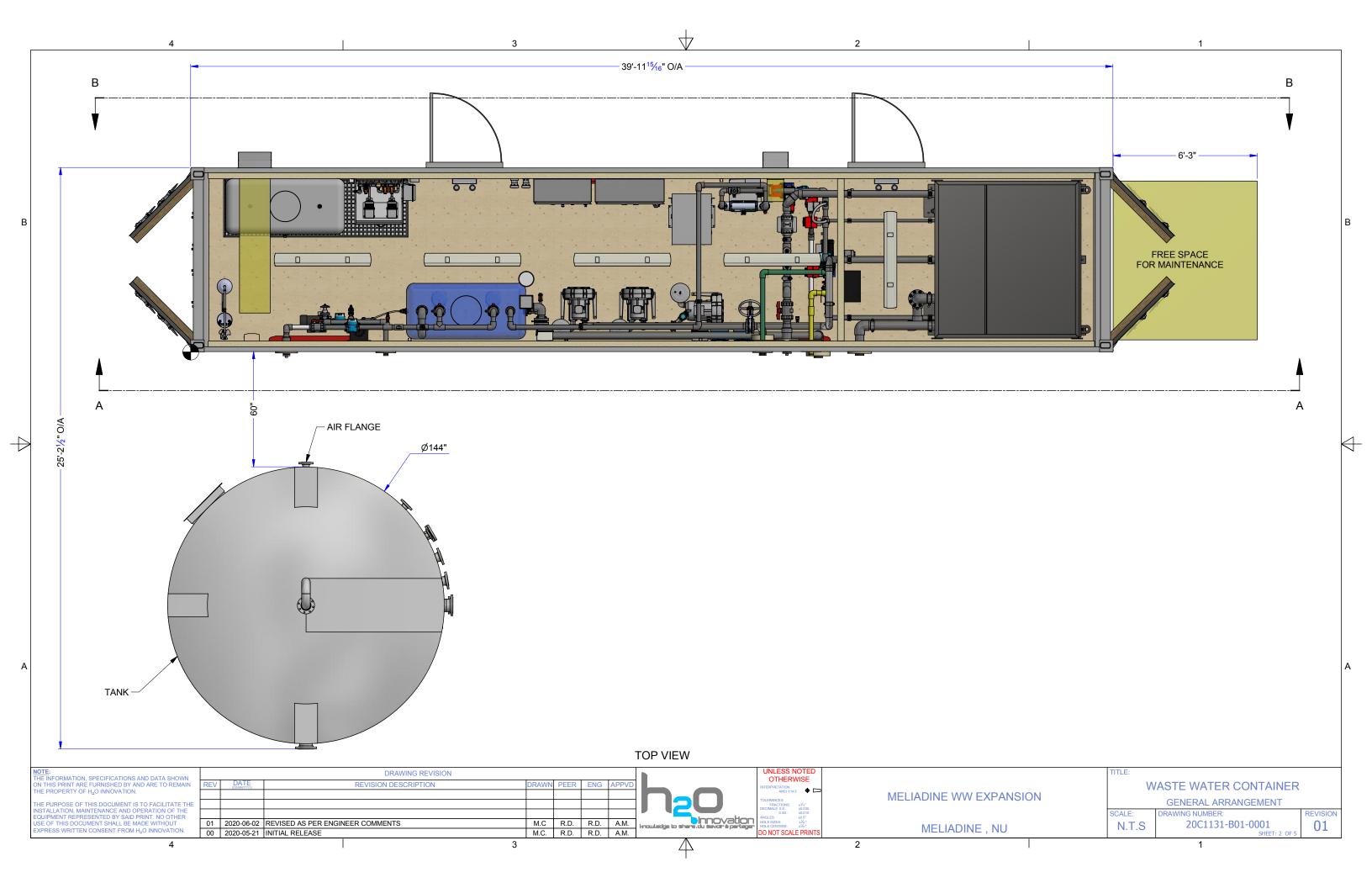
4.4 TIMELINE

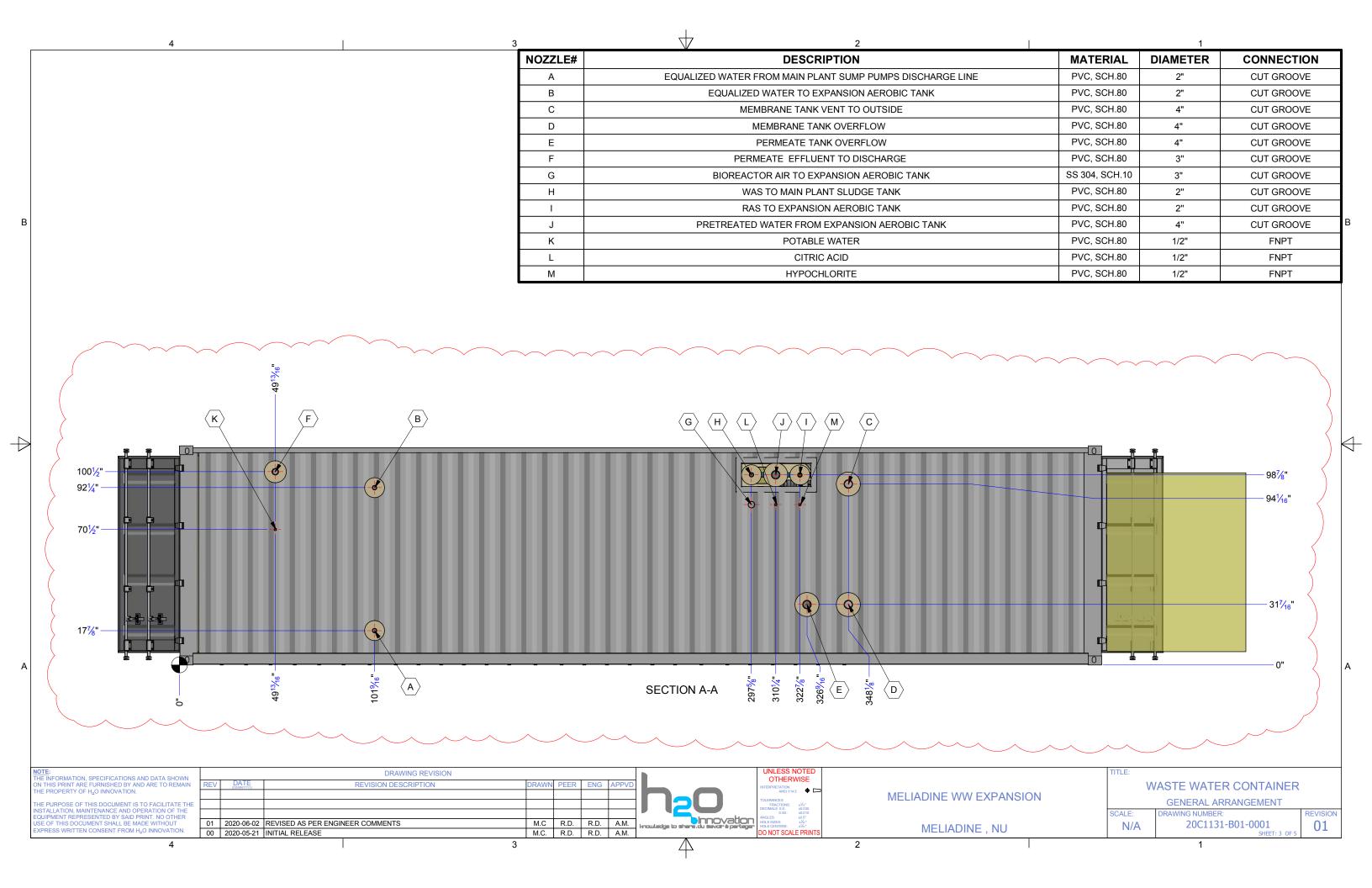
The expected date of construction is September 1st 2020, commissioning completion is planned for mid-September 2020.

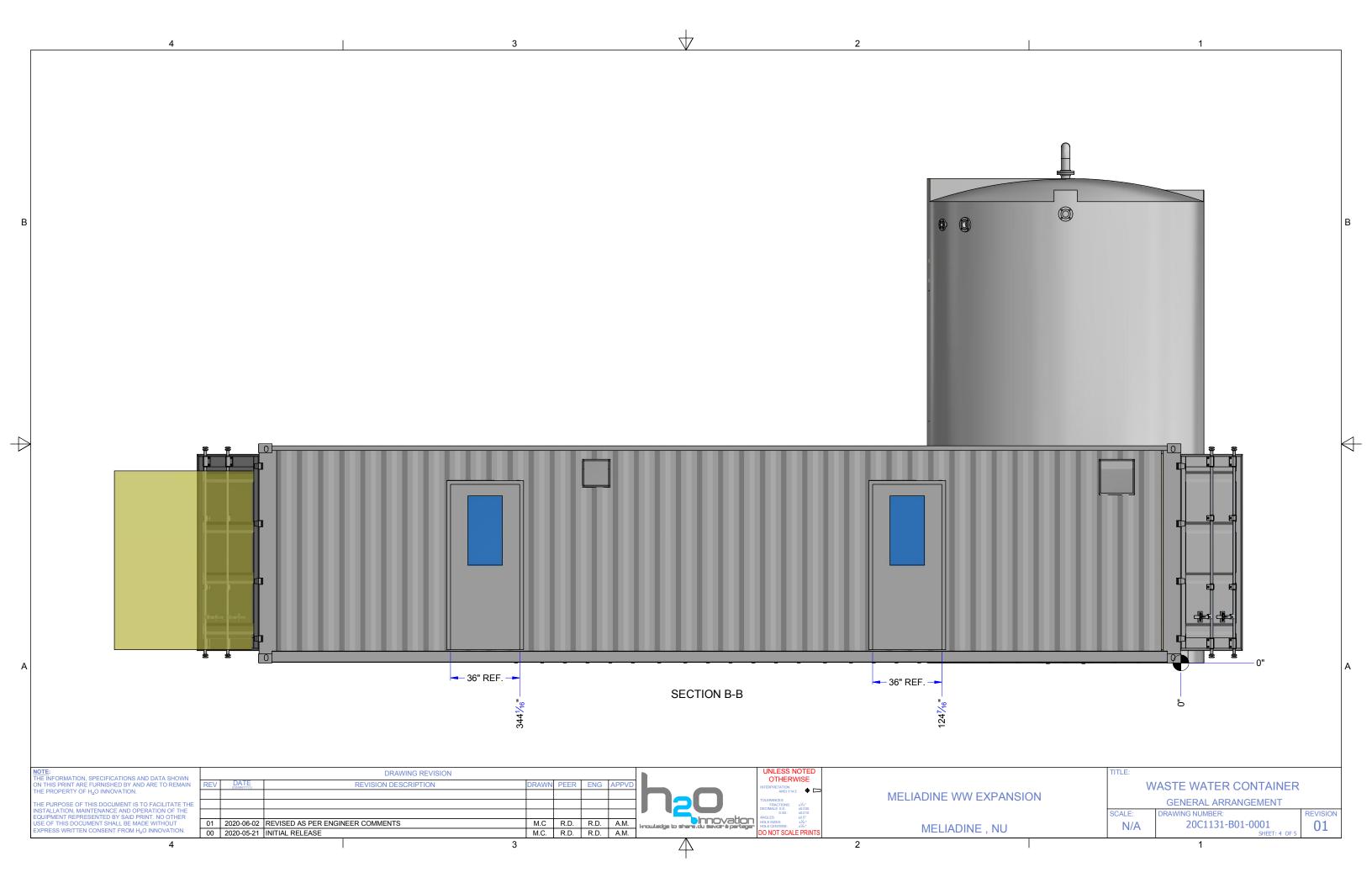
Appendix A : STP upgrade



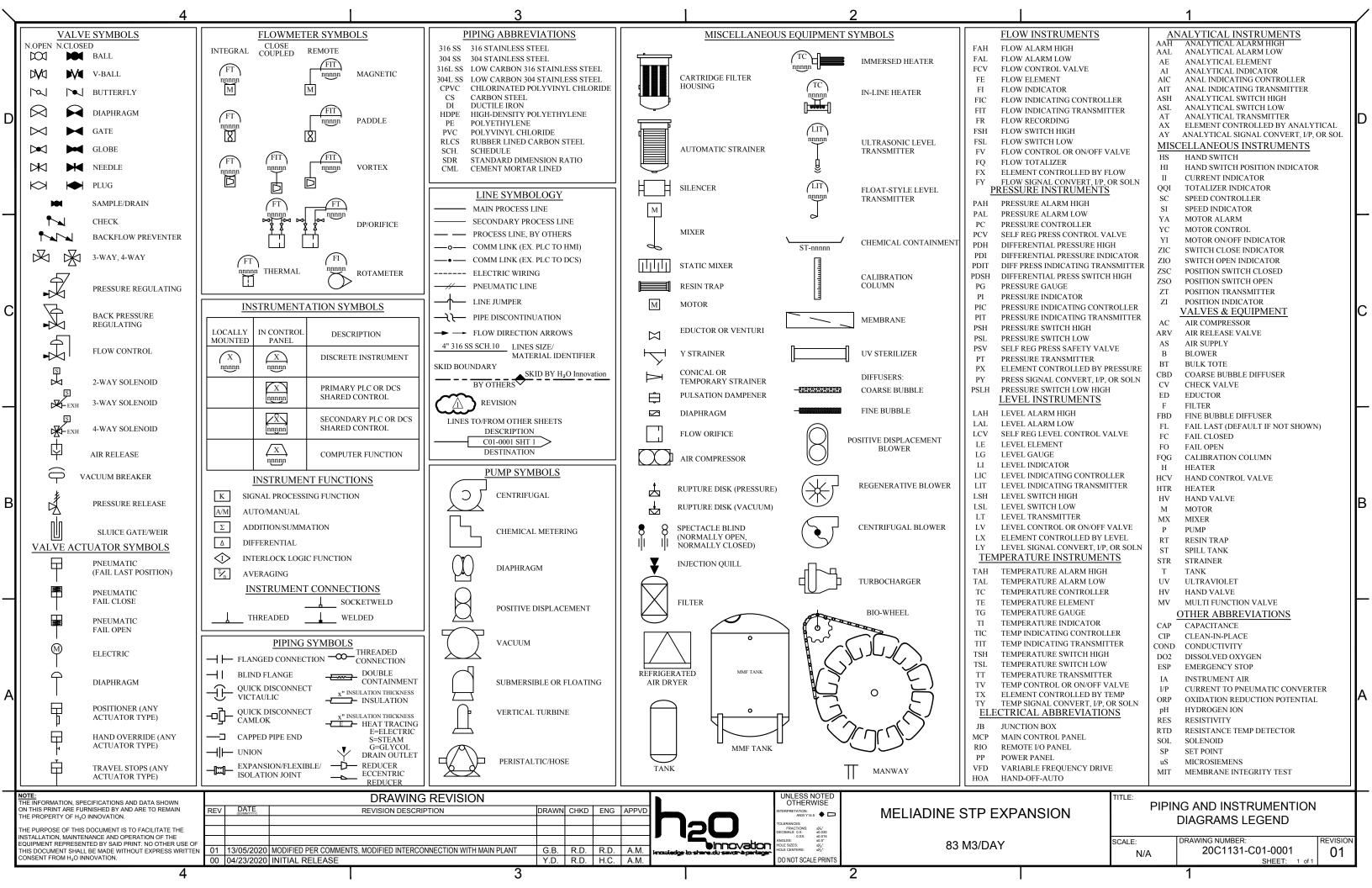


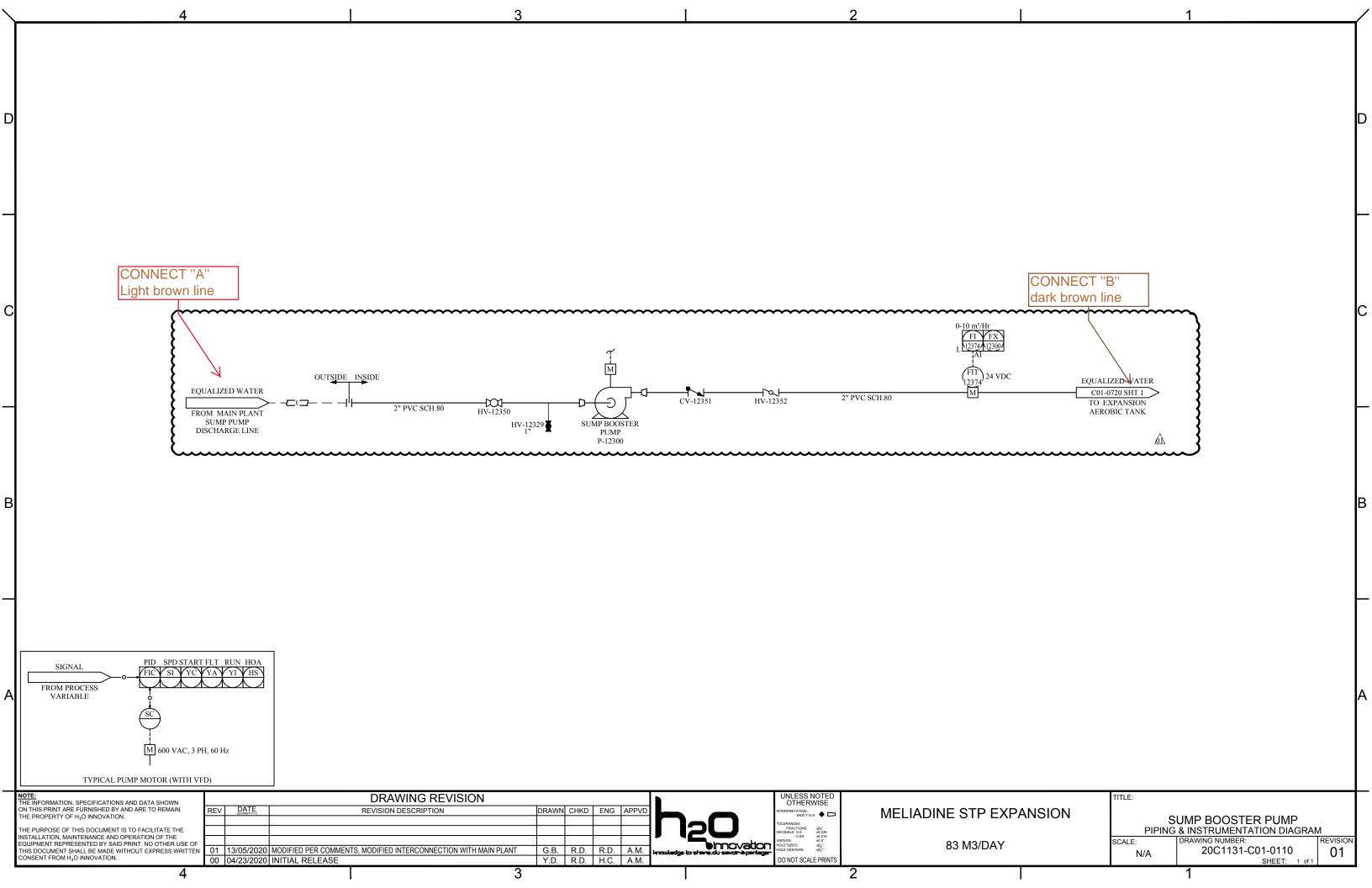


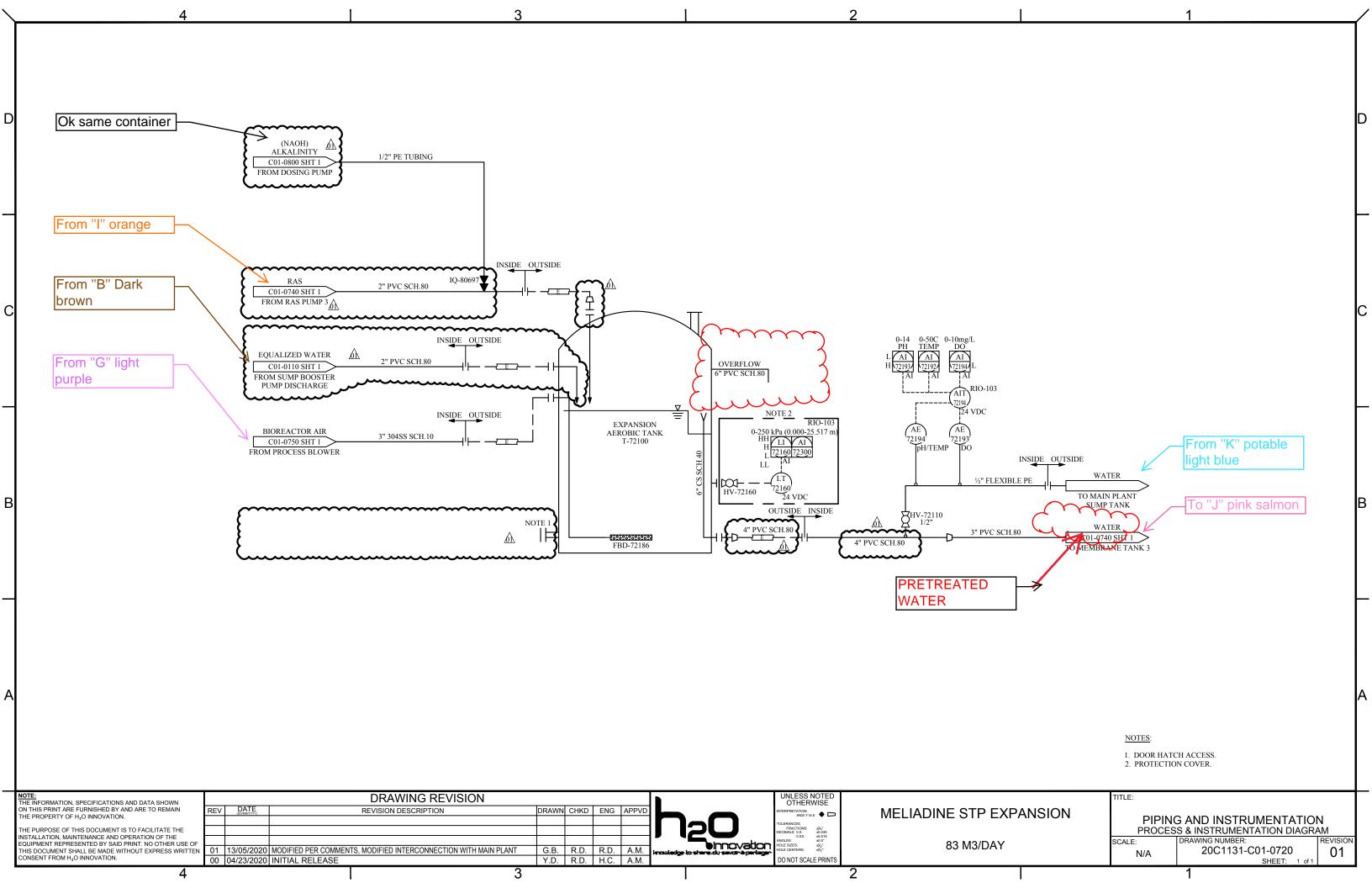


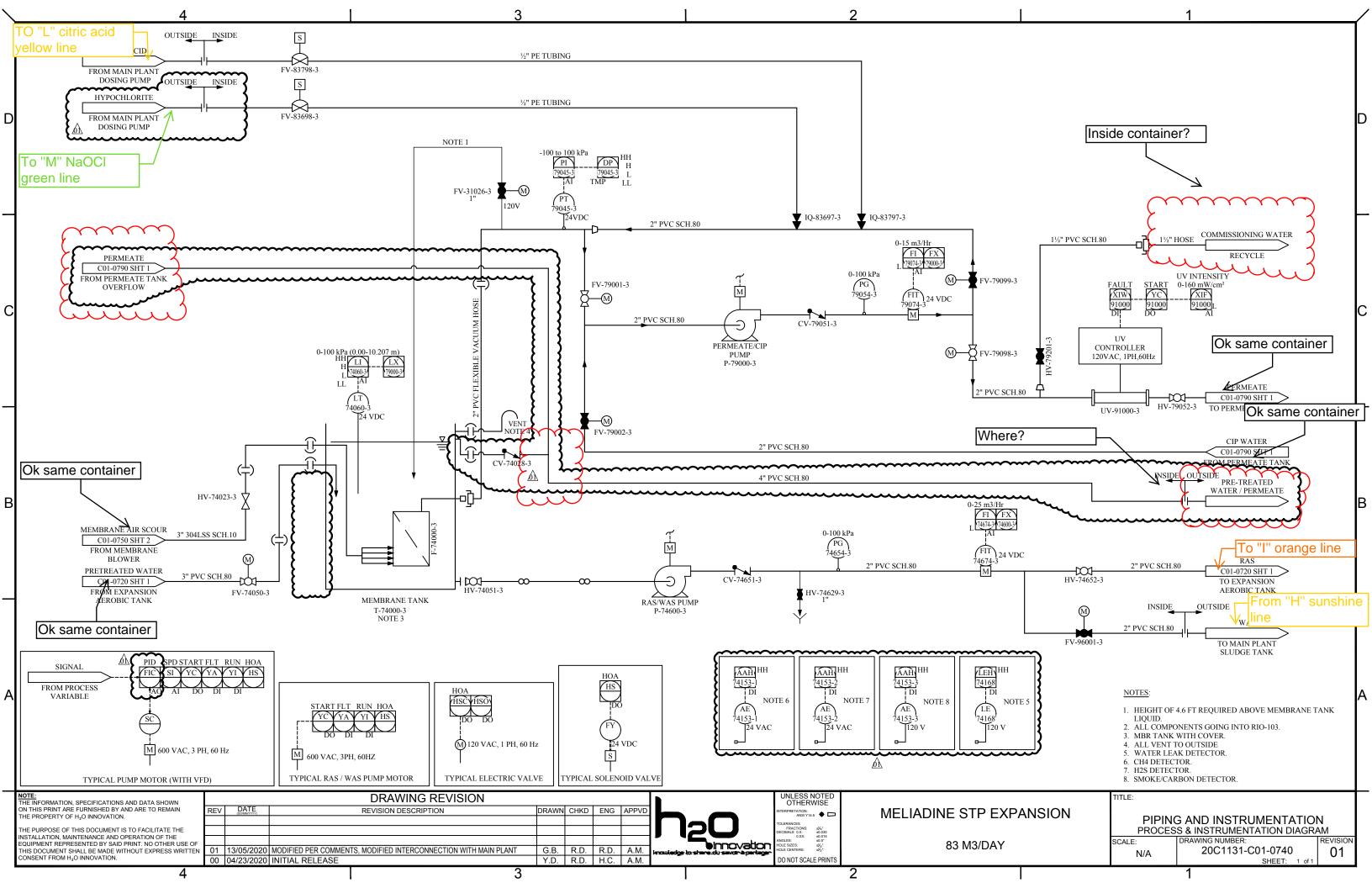


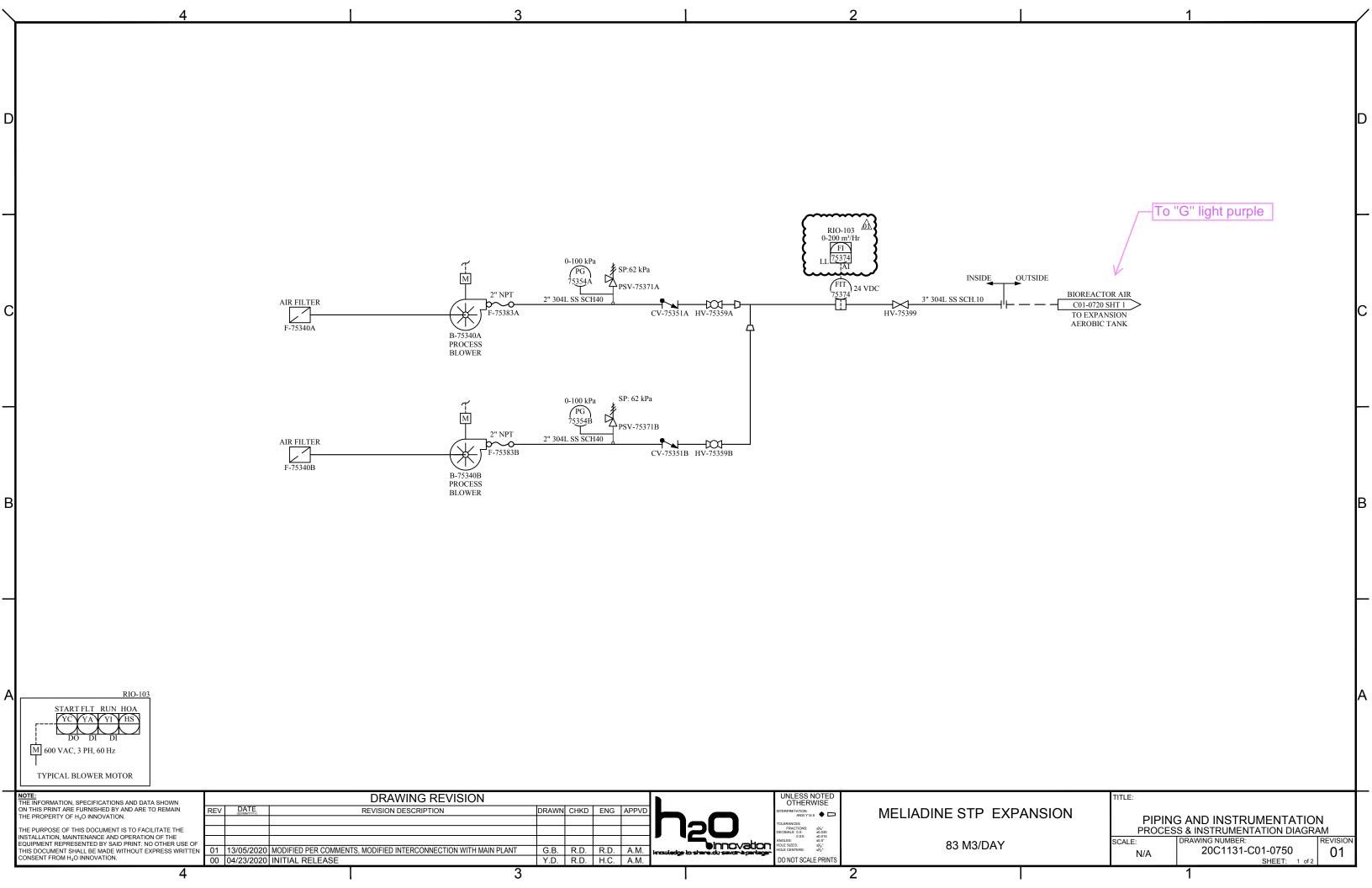
RAS PUMP INLET -3" FLANGE SCREENED WATER FROM SUMP PUMP -2" FLANGE FROM BLOWER 3" FLANGE TO MEMBRANES TANK -FLANGE 6" *** O O O O - 144" — RIGHT VIEW BLIND FLANGE WITH TAPED HOLE 1/2"-14 NPT FRONT VIEW NOTE:
THE INFORMATION, SPECIFICATIONS AND DATA SHOWN ON THIS PRINT ARE FURNISHED BY AND ARE TO REMAIN THE PROPERTY OF H₂O INNOVATION. DRAWING REVISION TITLE: OTHERWISE REVISION DESCRIPTION WASTE WATER CONTAINER MELIADINE WW EXPANSION THE PURPOSE OF THIS DOCUMENT IS TO FACILITATE THE INSTALLATION, MAINTENANCE AND OPERATION OF THE EQUIPMENT REPRESENTED BY SAID PRINT. NO OTHER USE OF THIS DOCUMENT SHALL BE MADE WITHOUT EXPRESS WRITTEN CONSENT FROM H₂O INNOVATION. GENERAL ARRANGEMENT DRAWING NUMBER: SCALE: Innovation
Anoutedge to share du savoir à partager 01 2020-06-02 REVISED AS PER ENGINEER COMMENTS 00 2020-05-21 INITIAL RELEASE 01 M.C R.D. R.D. A.M. 20C1131-B01-0001 N/A MELIADINE, NU M.C. R.D. R.D. A.M.

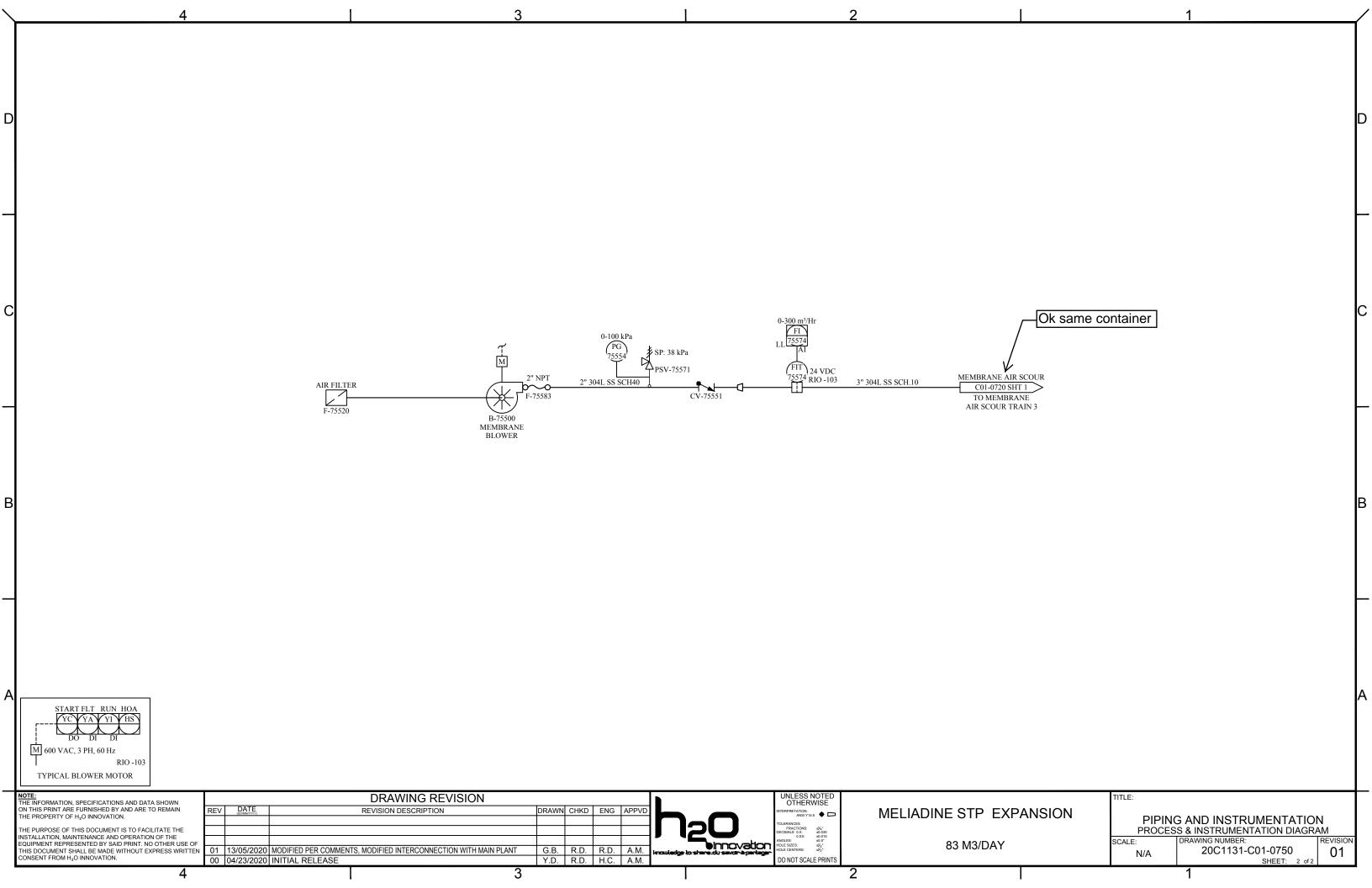


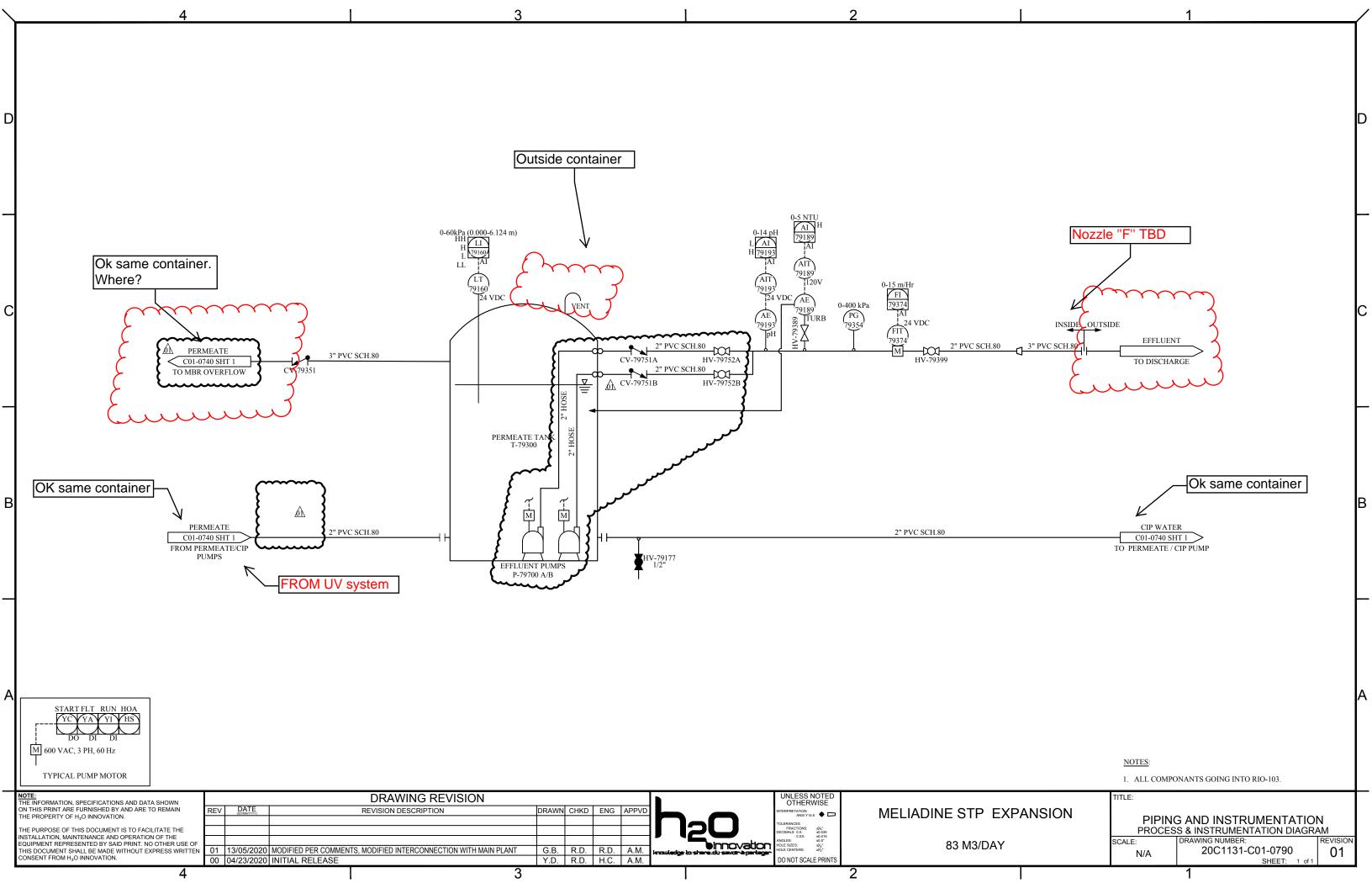


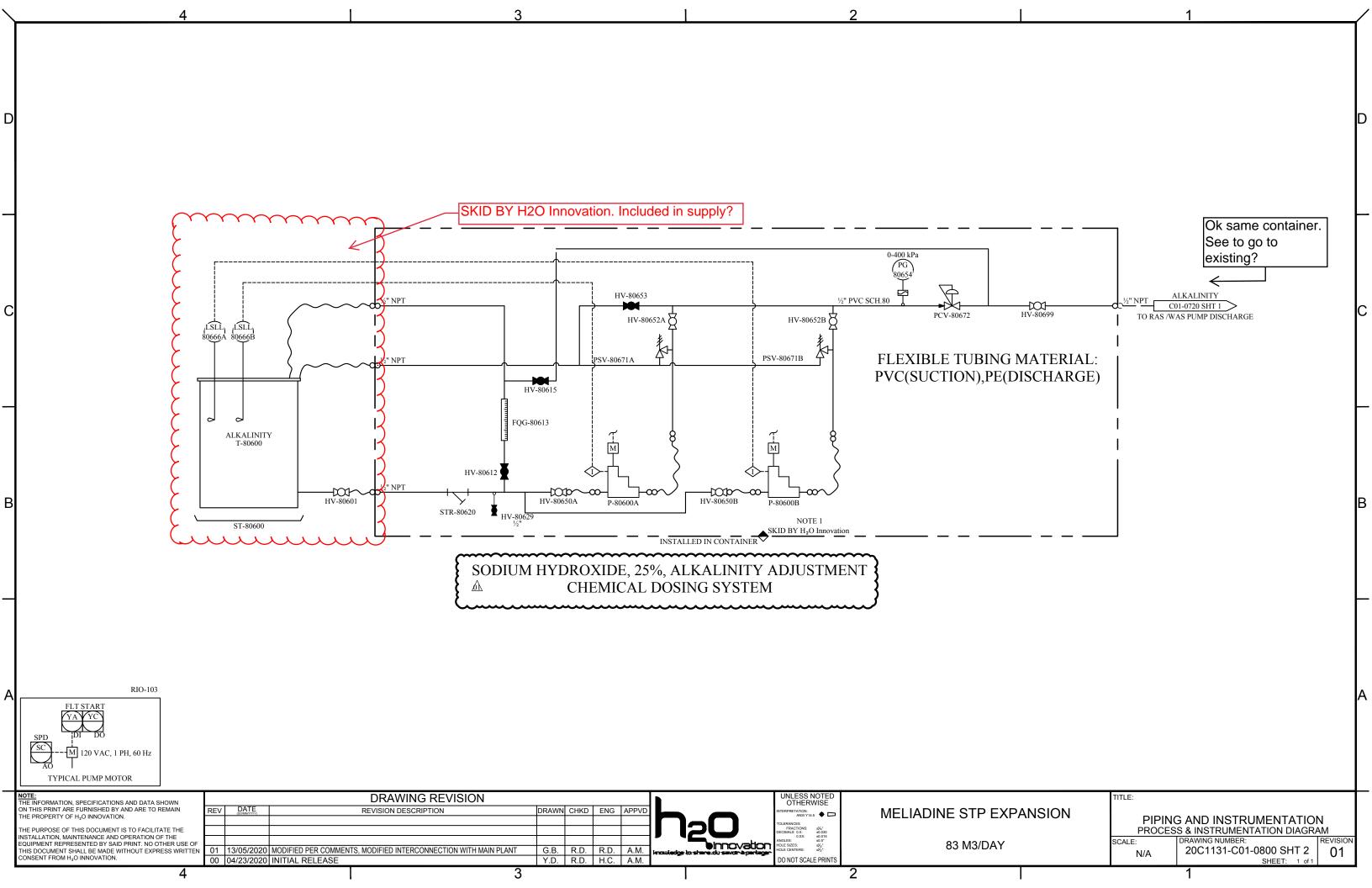












Appendix B : Current STP

