

January 19th 2017

Karen Kharatyan Manager of Licensing Nunavut Water Board P.O. Box 119 Gjoa Haven, NU X0B 1J0

Re: Water License 2AM-MEL1631 Part D, Items 1&2 - Submission of Final Design and Construction Drawings for the Sewage Treatment Plant

Mr. Kharatyan,

Agnico Eagle Mines Limited is developing the Meliadine Project, a gold mine located approximately 25 km north from Rankin Inlet, and 80 km southwest from Chesterfield Inlet in the Kivalliq Region of Nunavut. Situated on the western shore of Hudson Bay, the Project site is located on a peninsula between the east, south, and west basins of Meliadine Lake (63°1'23.8" N, 92°13'6.42"W) on Inuit Owned Land.

Facilities that are planned to be constructed for the operation of the future Meliadine Mine include a mill, power plant, maintenance facilities, tank farm for fuel storage, water treatment plant, sewage treatment plant, and accommodation and kitchen facilities for 520 people.

In accordance with Water License 2AM-MEL1631, Part D, Items 1 and 2, please find enclosed with this letter, a copy of the final design and construction drawings for the Sewage Treatment Plant.

Should you have any questions regarding this submission, please contact me.

Regards,

Agnico Eagle Mines Limited - Meliadine Division

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cc: Ian Parsons, Indigenous and Northern Affairs Canada Luis Manzo, Kivalliq Inuit Association



Meliadine Sewage Treatment Plant

30-Day Notice to Nunavut Water Board In Accordance with Water License 2AM-MEL1631 (Part D, item 1)

Prepared by:
Agnico Eagle Mines Limited – Meliadine Division





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1 INTRODUCTION

1.1 SITE LOCATION AND ACCESS

Agnico Eagle Mines Limited (Agnico Eagle) is developing the Meliadine Project (the Project), a gold mine located approximately 25 km north from Rankin Inlet, and 80 km southwest from Chesterfield Inlet in the Kivalliq Region of Nunavut. Situated on the western shore of Hudson Bay, the Project site is located on a peninsula between the east, south, and west basins of Meliadine Lake (63°1'23.8" N, 92°13'6.42"W) on Inuit Owned Land.

The area is accessible from the all-weather gravel road linking the existing exploration camp with Rankin Inlet.

1.2 EXISTING AND FUTURE SITE FACILITIES

Current facilities at the Meliadine Project site include the exploration camp located on the shore of Meliadine Lake, approximately 3.5 km south-east of the future accommodations. The self-contained exploration camp consists of four wings of new trailers that can accommodate up to 200 people and includes kitchen facilities, complete with diesel generators. Power for the exploration camp is currently provided by diesel generators. Potable water for the exploration camp is pumped from Meliadine Lake.

Facilities that are planned to be constructed for the operation of the future Meliadine Mine include a mill, power plant, maintenance facilities, tank farm for fuel storage, water treatment plant, sewage treatment plant, and accommodation and kitchen facilities for 520 people.

The Nunavut Water Board (NWB) has issued Type A Water License 2AM-MEL1631 to Agnico Eagle Mines Limited (Agnico Eagle) for the Meliadine Gold Project site authorizing the use of water and the disposal of waste required by mining and milling and associated uses.

This report includes the final design and construction drawings for the sewage treatment plant (STP), as specified under Water License 2AM-MEL1631 Part D, Item 1.

Figure 1 shows the location of the future STP and pipeline to CP1 for final discharge.



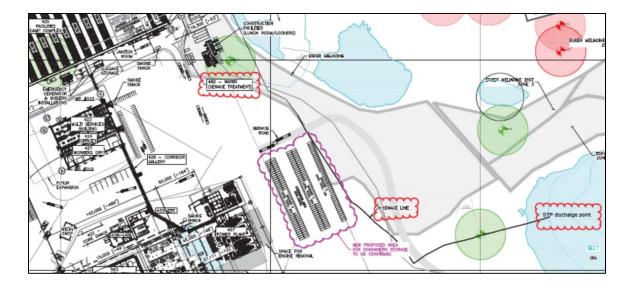


Figure 1 –Location of Meliadine STP and effluent pipeline to CP1 (former dewatered Pond H17)



2 DESIGN

2.1 WATER MANAGEMENT STRATEGY

Sewage will be collected from the new facilities and pumped to the new STP. In addition to the sewage generated from the buildings connected to this STP, a sewage vacuum truck will collect sewage from storage tanks at different temporary or remote buildings such as the emulsion plant, the paste plant, the crusher building, the portal #1 and construction offices. This material will be directly deposited into in the STP equalization tanks.

The objective of the STP is to treat sewage to an acceptable level for discharge to CP1 via a sewage water discharge pipeline. The STP is housed in a prefabricated (modular) structure, located on the east side of the industrial pad (Figure 1). The sewage treatment system is designed for a maximum daily flow rate of 216 m³ and a peak hour flow of 106 m³, and an average Biological Oxygen Demand (BOD) in the influent of 200-360 mg/L.

The treated sewage from the STP will be pumped through a heat traced insulated pipeline to CP1 pond which is designed to receive all the surface contact waters on site. This water is pumped to the final effluent treatment plant for TSS control prior to discharge into Meliadine Lake.

The composition of the sewage and grey water entering the plant and the composition water exiting the units will be monitored on a regular basis to determine plant efficiencies.

Sewage sludge removed from the STP will be added to the landfarm as nutrient amendment on an as needed basis. Excess sludge will be disposed of in the Tailings Storage Facility (TSF) or shipped south for disposal.

2.2 DESCRIPTION OF SEWAGE TREATMENT SYSTEM

The STP relies on bacterial activity. The process is composed of five (5) steps described below: screening and flow equalization, aerobic biological treatment, membrane filtration, ultraviolet disinfection, and sludge handling. The flow diagram is available in Appendix B.

2.2.1 Screening and Flow Equalization

Influent wastewater is pumped to the two (2) aerated equalization tanks. The equalization system is able to manage a variation in flows. It provides raw wastewater storage of up to 50% of the design flow to store feed during high flow periods and to ensure feed supplementation during low flow periods. It provides a stable and consistent raw feed for the downstream processes. Equalized water is pumped via two (2) equalization pumps into a standpipe inside the second tank and flows from that pipe by gravity to the fine screens. The fine screens are rotary drum screens with 2 mm perforated plate openings that operate continuously. The screens will ensure the removal of large debris to protect downstream equipment. Pressurized wash water is used intermittently to clean the screens and screenings.





2.2.2 Aerobic Biological Treatment

Screened raw water falls by gravity from the screens into the sump tank, where it is pumped to the aerobic tank, which is located outdoors. Aerobic biological treatment remove the organic load (measured as BOD) of the wastewater. Bacteria grown in the bioreactor remove unwanted organic pollutants to produce a treated water of high quality. Oxygen is supplied by regenerative blowers and is injected by fine bubble diffusers in the tank. The diffusers are designed for a wide range of air flows, according to the system's demand in oxygen. It keeps a dissolved oxygen concentration of at least 2 mg/L at any time to satisfy the needs of the biomass. The mixed liquor suspended solids (MLSS) overflows into a standpipe inside the tank and flows by gravity to the membrane filtration trains.

The dry bacteria product, BEC105, could be used in the treatment process to stimulate biological activity when needed.

2.2.3 Membrane Filtration System

Membrane filtration is used to separate the bacteria from the water to ensure keeping them in the process at the desired concentration. Activated sludge is returned at a constant flow rate to the aerobic tank to prevent a build-up of sludge in the membrane tank. The return activated sludge (RAS) is pumped at a higher flow rate than the design flow rate of the plant, to make sure that there is good circulation in the whole system and that there is no accumulation of solids.

The membranes are totally submerged and have a pore size of 0.4 microns, which remove all suspended solids in the effluent.

Permeation pumps are provided to suction the effluent through the membrane modules and transport it to the permeate tank. Permeation pumps are supplied with variable speed drives to overcome any changes in transmembrane pressure and achieve the design at all times.

The operating cycle for the selected modules is to suction effluent water for seven (7) minutes and to relax the membrane for one (1) minute. The cycle optimizes the long-term operation of the membrane modules. The housings are constructed with an integrated diffuser at the bottom to aerate continuously the membrane and prevent clogging and accumulation of sludge. The relaxation of the membranes allows extending the interval between cleanings (CIP or Clean-In-Place). CIP cleans are done about twice a year. Washes are performed with permeate stored in the permeate storage tank while a cleaning chemical (either sodium hypochlorite or citric acid) is added. Chemical solutions are reverse flowing through the membranes, which are soaked for a few hours after. After washing, the permeation is restarted. While a train is washing, the other train can continue to treat water and ensure a continuous production of effluent.

Once a week, a chemically enhanced backpulse (CEB) should be performed on the membrane modules with sodium hypochlorite to mitigate membrane fouling. Permeate flow is reversed to flow back into the membranes while the cleaning chemical is added inline.





2.2.4 UV Disinfection System

From the permeate pumps, each membrane bioreactor train sends permeate through an inline ultraviolet disinfection system. It is a physical process that inactivates instantaneously microorganisms. The UV system process adds no chemicals to the water, and therefore, has no impact on the chemical composition of the effluent. From here, effluent is sent to a common permeate storage tank. The permeate tank acts as a reservoir for treated water that is pumped to a discharge location. This tank can also be used for CEB and CIP process, as previously mentioned.

2.2.5 Sludge Handling System

Since bacteria continue to reproduce as the consume organics and nutrients, the concentration of biomass, measured as Mixed Liquor Suspended Solids (MLSS), increases with time. Periodic sludge wasting is required to control the MLSS concentration in the bioreactor tanks.

Sludge is sent to the sludge storage tank by redirecting the flow of the RAS pump. A blower and coarse bubble diffuser system maintains an aerobic environment within the sludge tank to minimize the proliferation of odours. Periodic settling is used to facilitate the thickening of the waste activated sludge. The supernatant (upper portion of the tank) is sent back to the sump tank by opening a valve, where it will re-enter the treatment process. This operation (called decanting) reduces the volume of sludge that needs to be handled and extends the period of time that the sludge tank can be used before thickened sludge is disposed.





3 DRAWINGS AND SKETCHES

Drawings of the new STP are available in Appendix A.



Appendix A: Sewage Treatment Plant Design Drawings

