

Based on the Meadowbank equipment design, it is expected to produce for the design criteria of 500 m³/h of feed water at 500 ppm TSS, approximately 446 m³/h of clarified water below 15 ppm TSS and 54 m³/h of sludge at 0.5% solid.

4.2 Actiflo®

The Actiflo® clarifier uses sand ballasted settling, a high rate coagulation-flocculation-sedimentation process. In the coagulation basin, TSS are destabilized under the action of the coagulant and start to form small aggregates (also called flocs). The coagulant is a trivalent soluble metal compound, usually iron or aluminum, which will cause coagulation when it reaches a certain concentration. Once the coagulant has performed the destabilizing effect, it will precipitate as a metal hydroxide and will participate in the formation of the aggregates. Water then flows into a second tank called the injection tank. There, micro-sand and polymer are added. The polymer acts as a flocculant aid, binding the destabilized solids together with the micro-sand particles by forming polymer bridges. The micro-sand provides a large contact area for floc attachment and acts as a ballast, thereby accelerating the settling of the flocs. From the injection tank, water flows into the maturation tank where flocs formed in the previous stage agglomerate and grow into high density flocs known as micro-sand ballasted flocs. Water then overflows to the settling section of the tank, and with the help of the lamella system, a solid-liquid separation is achieved resulting in clarified water exiting from the system via a collection trough or weirs. The clarified water is monitored for pH, turbidity and flow rate prior to final discharge. The flow rate signal is also connected to a flow totalizer.

The flocs settle in a portion of the system where they are collected by a rake mechanism. A proportion of the unit's design raw water flow is continuously withdrawn from the clarifier and pumped to a hydrocyclone system which separates the micro-sand from the sludge. The recovered micro-sand is reused in the process. A small quantity of the micro-sand is not recovered by the hydrocyclones and remains within the sludge. The lost micro-sand needs to be replaced periodically by adding more to the process. After micro-sand separation, the sludge is sent to discharge location point (expected solid content from 0.5 to 3 % solid depending on TSS feed water quality).

4.3 Service Water System

The service water system consists of two (2) multimedia filters, two (2) heaters, one (1) filtered water tank and two (2) service water pumps. Service water is used in the preparation of dry chemicals and for polymer makeup systems. The coagulant and polymer require filtered heated water. Treated water from the Actiflo® is used to produce service water.

4.4 Reagents

One (1) polymer as well as a coagulant is used to treat the water that flows through the Actiflo®, each is supplied by a dosing system that is adjusted according to the influent flow rate. Treated water from the Actiflo® is used for the mixing of the reagents.

The cationic polymer used is the: Hydrex 3613. Typical dosage are 1-2 ppm.

The coagulant used is the: Hydrex 3267 (poly aluminum salt). According to the supplier, for typical dosage (50 ppm), no pH correction with sodium hydroxide is expected.

4.5 Controls

The Actiflo® Feed Pump a diesel pump working on an ON/OFF mode that allows the flow to be constant during ON mode at 444 m³/h. The flow is monitored on the feed pipe of Actiflo®

The raw water TSS analyzer (turbidity sensor) is used to monitor the water quality. An alarm is triggered when a high-high turbidity is reached. The high-high turbidity alarm value is a setting that will be determined during the commissioning phase and will depend on the quality of the water to be treated.

The effluent water TSS concentration (turbidity) and pH values are monitored continuously with in-line instrumentation. If effluent concentrations reach a set point indicating that final effluent discharge criteria may be exceeded, an alarm is sent to the Operator, who will manage the system to meet effluent criteria. A second alarm is sent to the Operator if effluent concentrations reach a second set point that is just below the final effluent discharge criteria.

Addition of the two (2) required reagents are proportional to the influent water flow. Since this flow is constantly maintained, no manual adjustment is required. If the operator has to modify the influent water flow, adjustment of the reagent dosing system will be required to maintain the target dosage rate. The reagent dosing systems are equipped with pumps that maintain a constant flow rate when running at a constant frequency. The flow can be modified by changing the electric motor frequency.

The reagent dosing system is equipped with valves and graduated cylinders allowing the Operator to measure the addition rate of the reagent using a stop watch. The Operator will determine the required flow of a specific reagent by a formula based on influent flow rate. Based on this calculation, a manual adjustment to the reagent pump will be done in order to obtain the required dosage. Initially, the formula will be based on laboratory testing and will be adjusted accordingly to the treatment plant performance. With time and experience, operation performance may be improved based on the results obtained and sharing practices with other sites such as at Meliadine.

4.6 Sludge Management

Sludge at approximately 0.5% solid will be rejected into an energy disperser pad a minimum distance of 31 m from the Whale Tail Lake shore. Sludge will be discharge on an energy dispenser to avoid erosion of the tundra. Rockfill berm will be built to reduce velocity of the effluent flow to limit erosion of the lake shore. Sludge effluent will reach Whale Tail North Basin in between the Dike and the turbidity barrier number B.

Plan of the energy dispenser and the berm is provided in Appendix E.

4.7 Batch Plant Requirement

After the reception of Licence A, Agnico Eagle (AEM) plans to build the Whale Tail Dike that will allow for the mining of the Whale Tail pit. One of the construction activities consists of installing the secant piles on the center line of the Whale Tail dike to act as the impervious layer.

The secant piles are a series of cement piles secant to each other who act as an impervious barrier in the center of the dike. They are built in advance, by means of drilling, metal casings through the dike structure and anchoring them to bedrock. Later on, the casing is filled with cement then removed. For the project, a large quantity of cement is to be produced, by a nearby batch plant, to be poured into the casings. The quantity of water required to produce the cement to fill the secant piles is an average of 126 m³/day and a production peak of 210m³/day. The average production rate was estimate based on a construction schedule of 76 days (from August to November 2018).

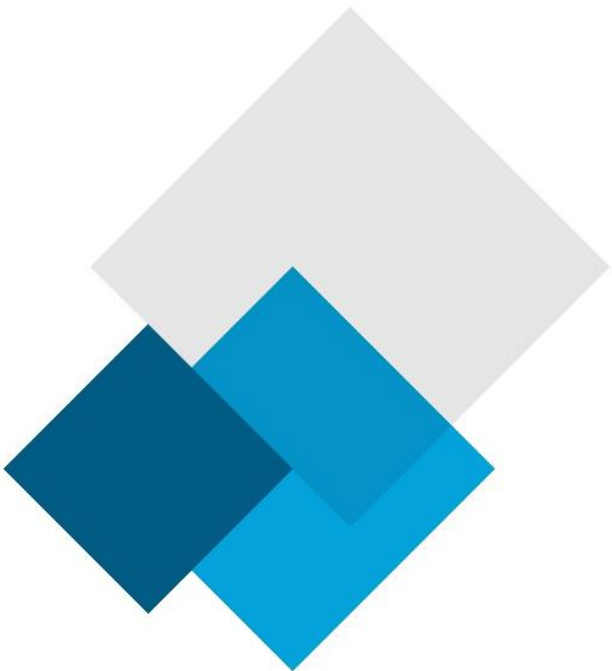
5. Pumping Station

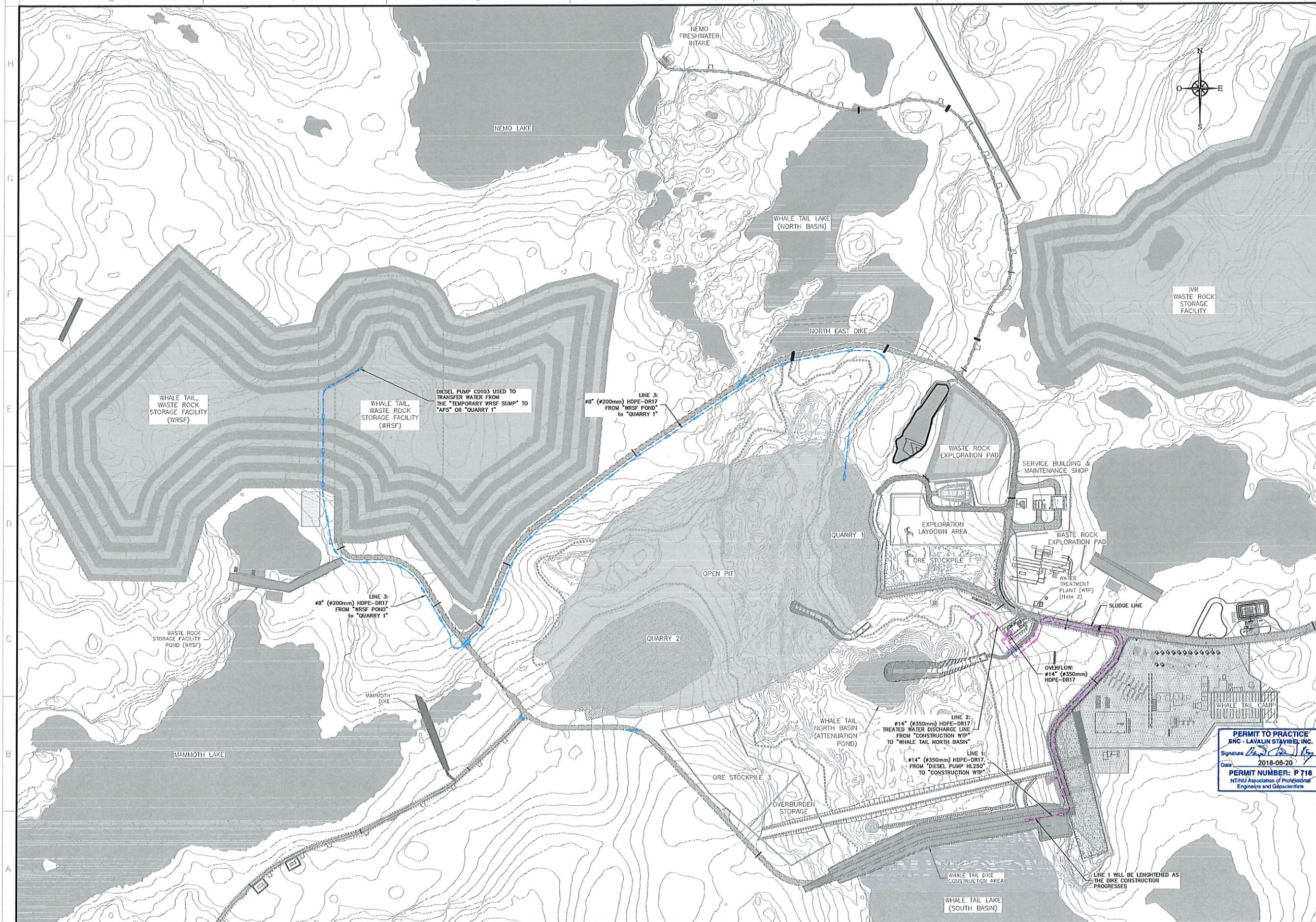
During the Whale Tail dike construction phase of the project, the main pumping requirements are the following:

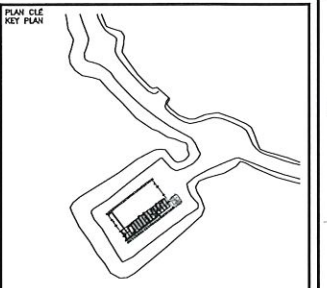
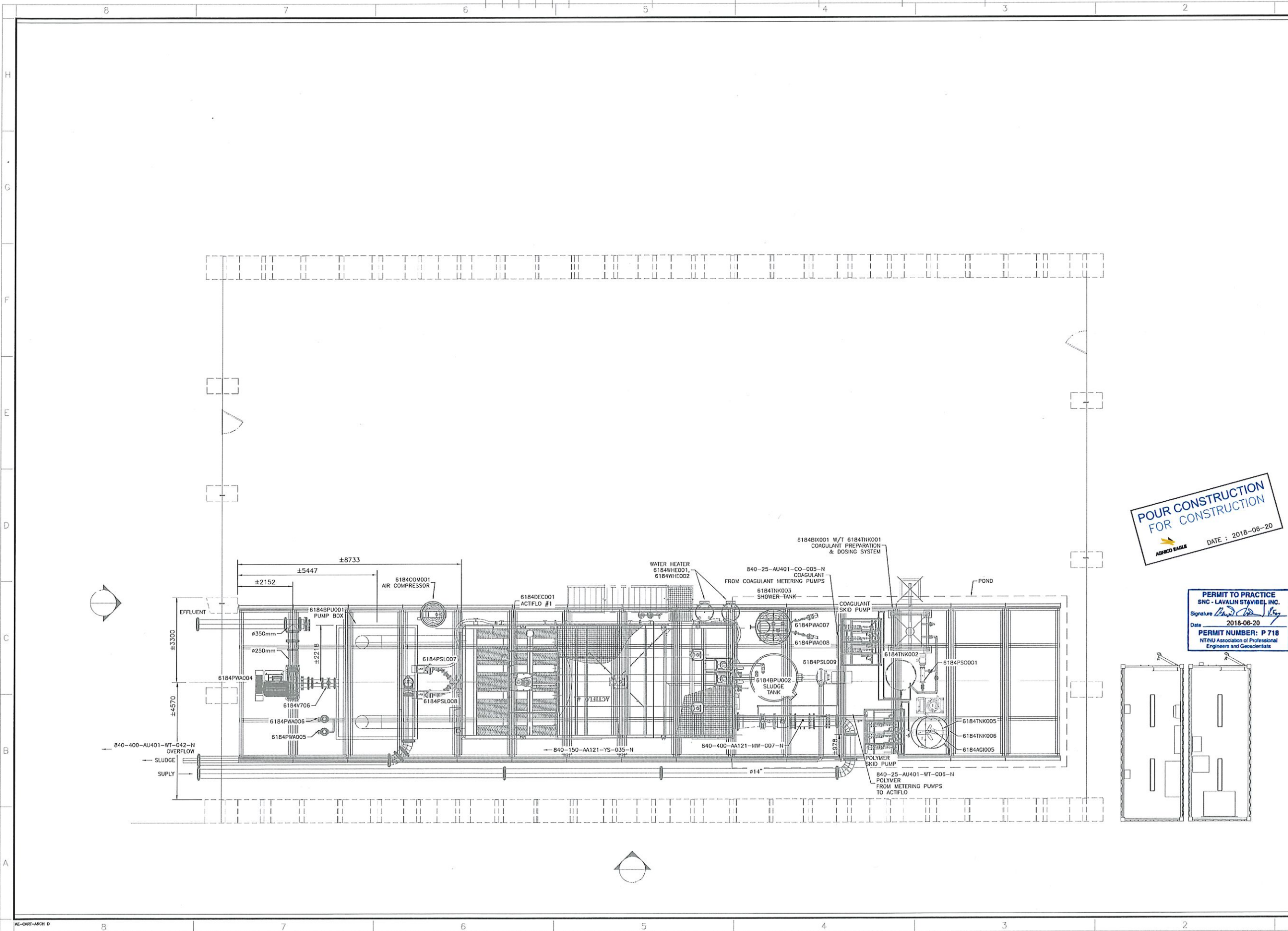
- › Transfer of contact water generated from the construction work on the Whale Tail Dike to the CWTP. The water will be collected between the first turbidity curtain and the dike that encircle the work area. This water will be pumped to the Construction Water Treatment Plant (CWTP) for treatment, primarily for Total Suspended Solid (TSS) removal.
- › Transfer of treated water from the CWTP to the Whale Tail North Basin.
- › Transfer of sludge from the CWTP to a rock fill structure located in the energy dispenser.
- › Pumping water from the North Whale Tail north basin to feed the batch plant used during dike construction.

Appendix A

Construction drawings



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TITRE / TITLE	#	CHG.

AGNICO EAGLE

AGNICO-EAGLE - WHALE TAIL
693 - FINAL WATER TREATMENT PLANT
210 - GENERAL ARRANGEMENT
LOCALISATION PLAN
WTP - ACTIFLO
RIGMAT

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REV.	DATE	DESCRIPTION	PREP.	APP.	CLIENT
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RIGMAT

DESIGNÉ PAR
DRAWN BY ERIC DENONCOURT, TECH. DATE 2018-04-27

VERIFIÉ PAR
CHECKED BY ISRAËL GAGNON, P.ENG. 2018-04-27

APPROUVÉ PAR
APPROVED BY BENOIT CHARTRAND, P.ENG. 2018-04-27

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SCALE NTS DATE 2018-04-27

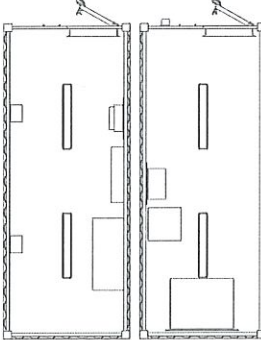
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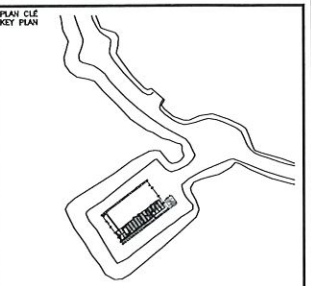
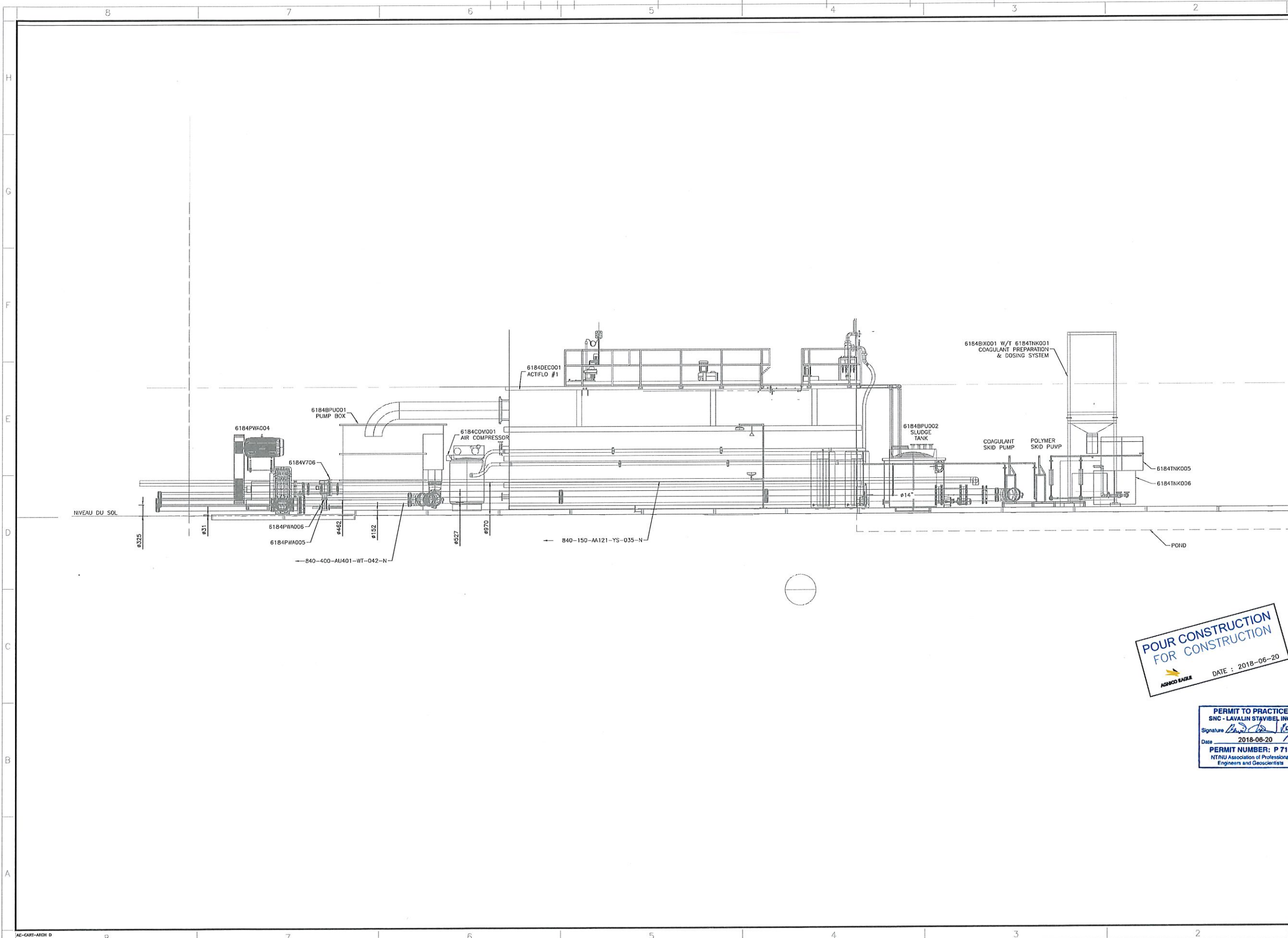
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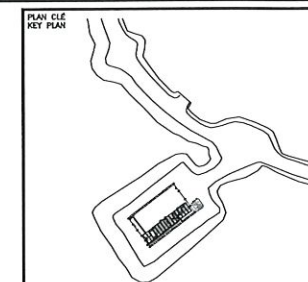
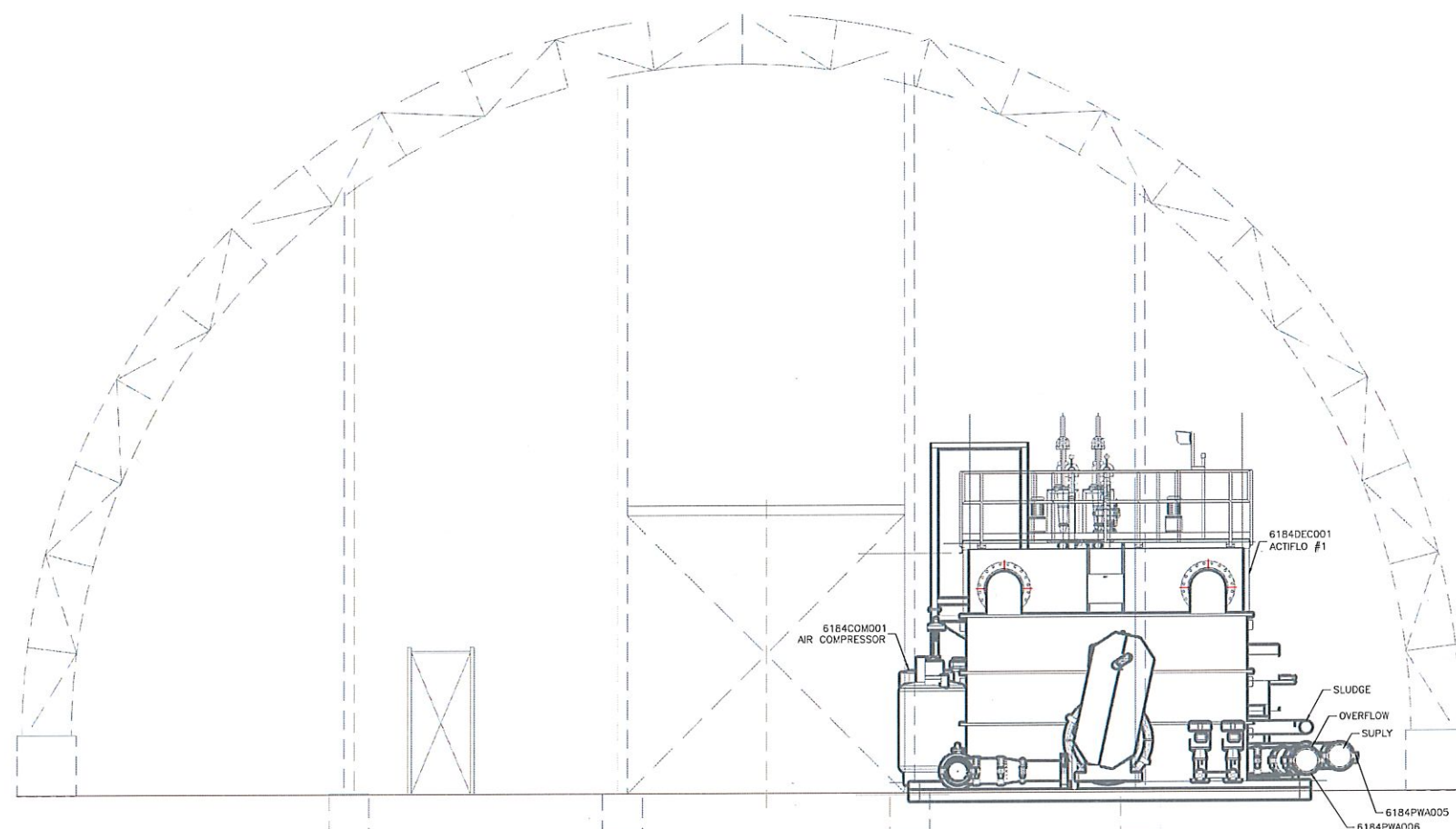
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APPROUVÉ PAR APPROVED BY	BENOIT CHARTRAND, P.ENG.	2018-04-27

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